

# Reducing Carbon Emissions in Gas Turbines using BASF OASE® Blue Technology

ETN Global - Webinar

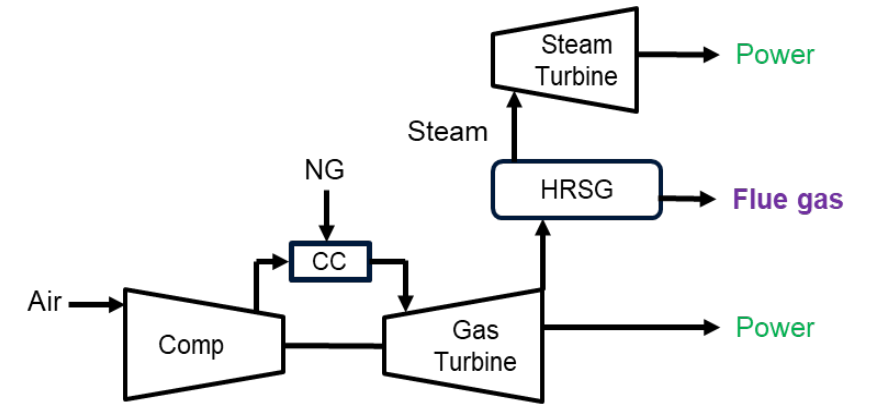
June 2024



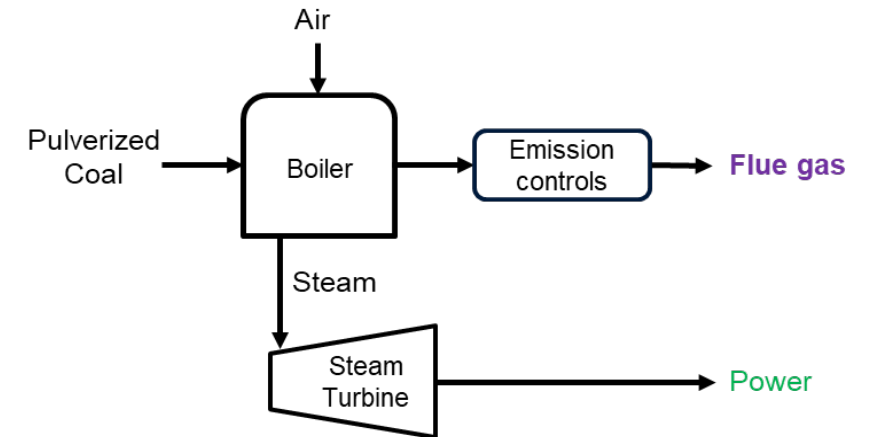
**OASE®**  
GAS TREATING EXCELLENCE

# Carbon Emission in Gas Turbines

- Power generation → biggest contributor of CO<sub>2</sub>
  - ▶ Coal and natural gas based
- Increasing investment in LNG projects → drive to produce carbon neutral LNG
- Shift to low carbon power generation → integration of CCS is critical
- Solvent based CO<sub>2</sub> capture is the most proven technology for CCS



Natural Gas Combined Cycle (NGCC) Plant



Coal-based Power Plant



**OASE® technologies**  
have been capturing  
carbon amongst  
other things since **1971**

white

Ammonia, Syngas

yellow

Sulfur Selective

**sulfexx™**

Super Selective

purple

Natural Gas, LNG

blue

Flue Gas

green

Biogas



**HiPACT**

Joint-development with JGC

**FLEXSORB™**

Strategic alliance with ExxonMobil

# OASE blue<sup>®</sup> Technology

- Solvent-based CO<sub>2</sub> capture technology
  - ▶ package of technology, solvent and services
  - ▶ Low regeneration energy & solvent make up
- Knowhow derived from +500 reference plants using OASE<sup>®</sup> technologies
- CO<sub>2</sub> capture from various flue gas applications:
  - ▶ Fossil fuel power generation
  - ▶ Cement / steel plant
  - ▶ SMR H<sub>2</sub> plant
  - ▶ Boilers



# Key Needs for Post-combustion CO<sub>2</sub> Capture

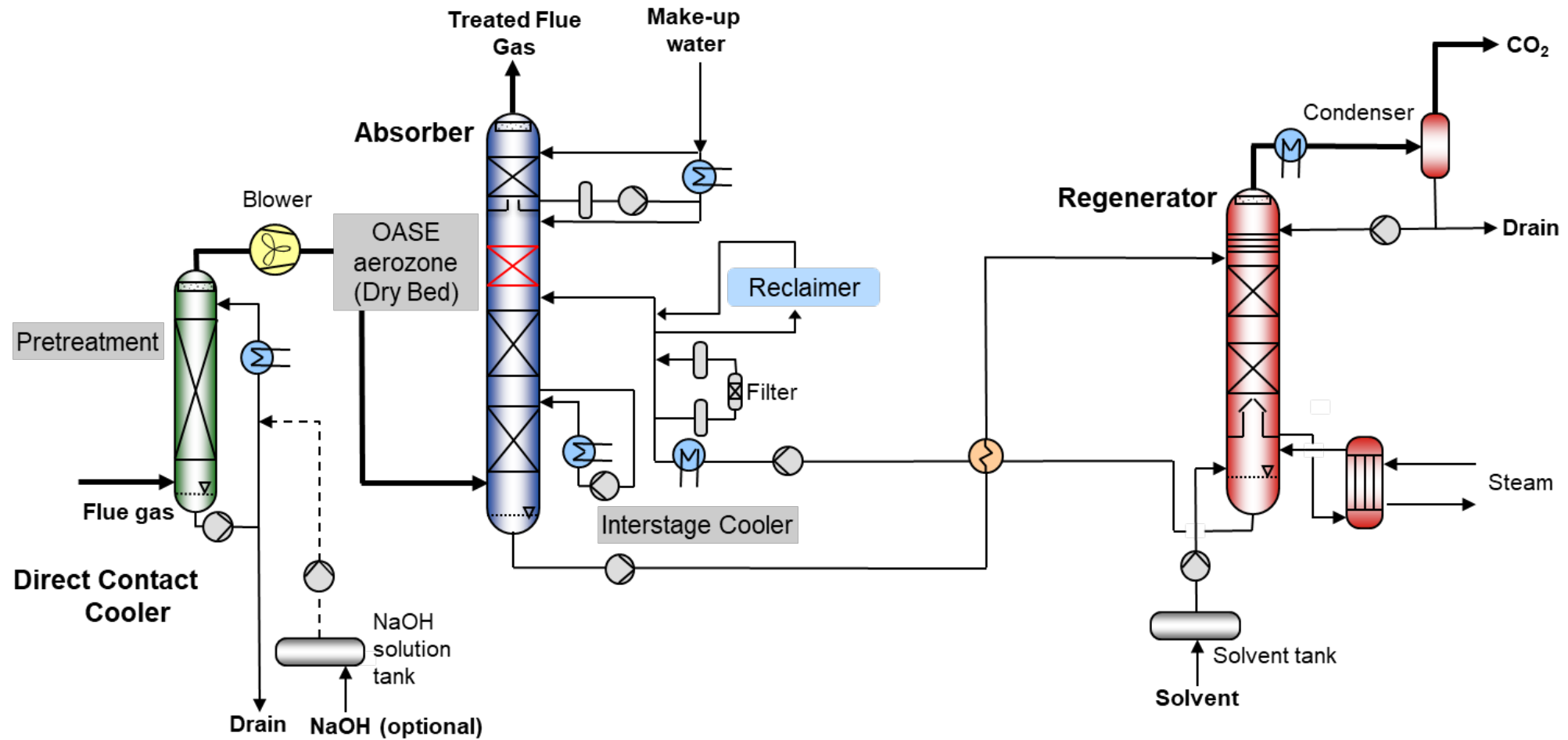
## Industry needs

- Proven technology
- High capture rates
- Low energy & amine consumption
- Low environmental impact
- Digitalization & operator friendliness
- Wide applicability
- Scaling & modularization
- Secure solvent supply

## BASF OASE® blue technology offering

- ⇒ Commercial references + over 65,000 hours of testing
- ⇒ CO<sub>2</sub> Removal Rate (up to **99%**)
- ⇒ **2.5 - 3.0 GJ/to<sub>CO2</sub>** / with solvent make up rate of **~0.3 – 0.6 kg<sub>amine</sub>/to<sub>CO2</sub>**
- ⇒ **OASE® aérozone** (Patented aerosol / emissions reduction zone)
- ⇒ Proven reclaimer concept
- ⇒ Nitrosamines management
- ⇒ **OASE® connect** (Design Software / Operators Training / Analytical DB)
- ⇒ **OASE® digilab** (Analyzer combined with OASE® connect)
- ⇒ Tested range O<sub>2</sub> (4 – 16 v%) / CO<sub>2</sub> (4 – 25 v%) / CO<sub>2</sub>
- ⇒ Easily scaled & modularized
- ⇒ Large scale solvent production

# OASE<sup>®</sup> blue Flow Scheme

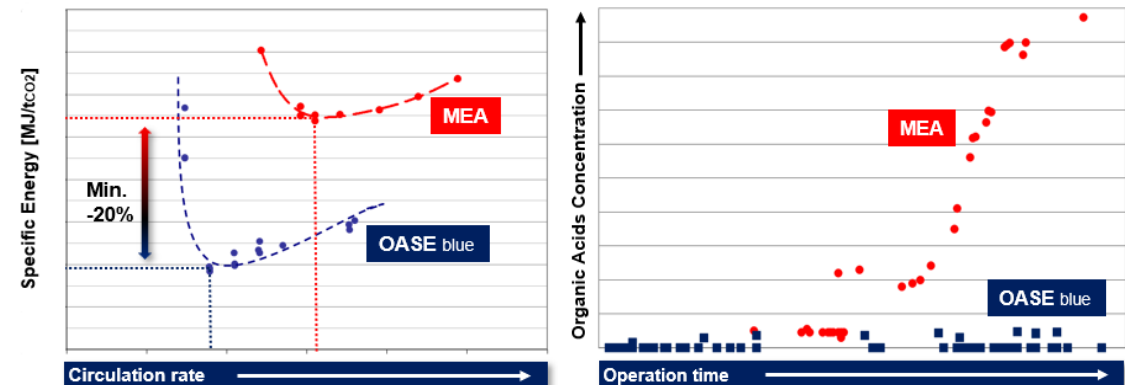


# Challenges : Flue Gas Composition

- Low CO<sub>2</sub> / O<sub>2</sub> ratio
  - ▶ Lower CO<sub>2</sub> kinetics
  - ▶ Higher degradation rate
    - Oxidative versus thermal degradation
    - OPEX consideration

Flue Gas	NGCC	Coal based power
Source	Natural gas	Pulverised coal
CO <sub>2</sub> (mol%)	3 - 6	12 - 15
O <sub>2</sub> (mol%)	10 – 16	3 - 8
Major impurities	NO <sub>x</sub>	NO <sub>x</sub> / Sulfur / Acidic Components / Metals
Dust /Aerosols	No / moderate	Yes

- OASE blue versus MEA
  - ▶ Minimum 20% saving in regeneration energy
  - ▶ > 70% make up rate saving

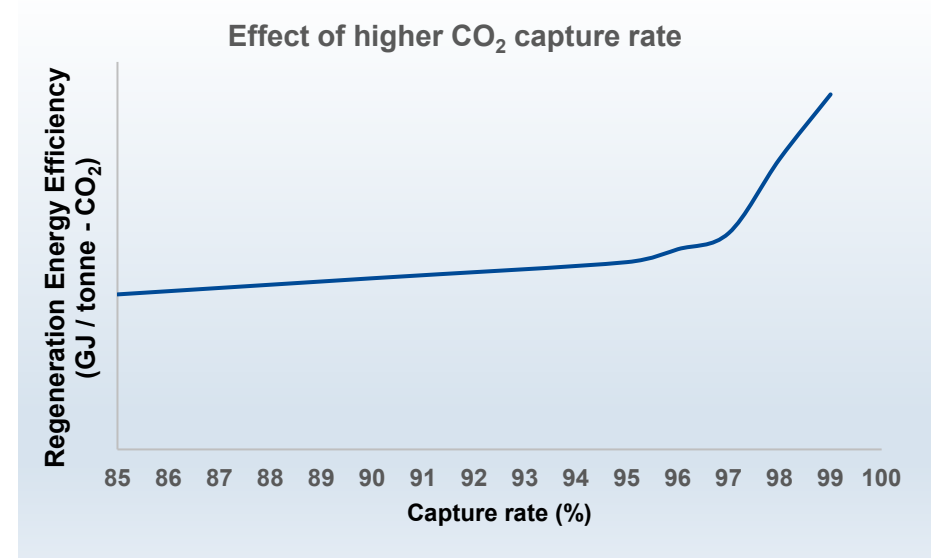
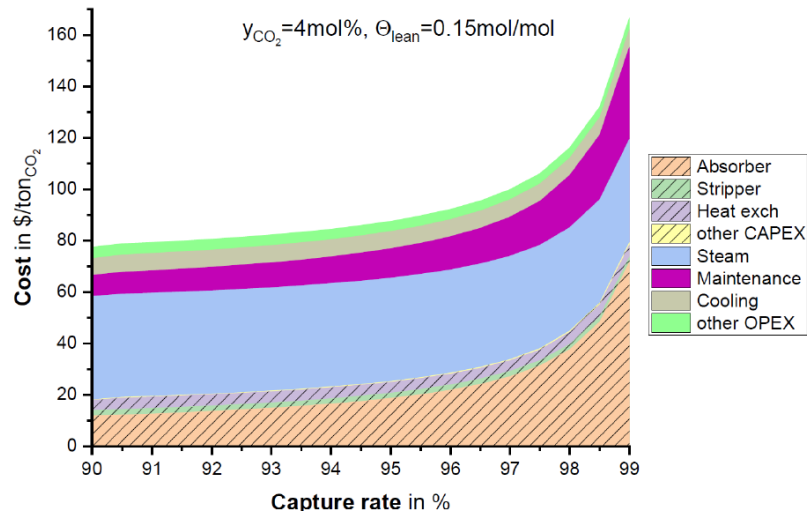


*Regeneration energy & make up rate comparison*



# Challenges : Capture Rate Efficiency

- Shifting capture rate benchmark to > 90%
- Major impacts to solvent-based CO<sub>2</sub> capture unit
  - ▶ Higher reboiler duty & cooling load
  - ▶ Higher solvent circulation flowrate
  - ▶ Bigger absorber diameter



- Theoretical study based on 30 wt% MEA
  - ▶ 90 – 98% capture → utility cost (OPEX)
  - ▶ Above 98% capture → absorber diameter (CAPEX)

Brandl, P., Bui, M., Hallett, J. P. & Mac Dowell, N. (2021). Beyond 90% capture: Possible, but at what cost? *International Journal of Greenhouse Gas Control*, 105, 103239.

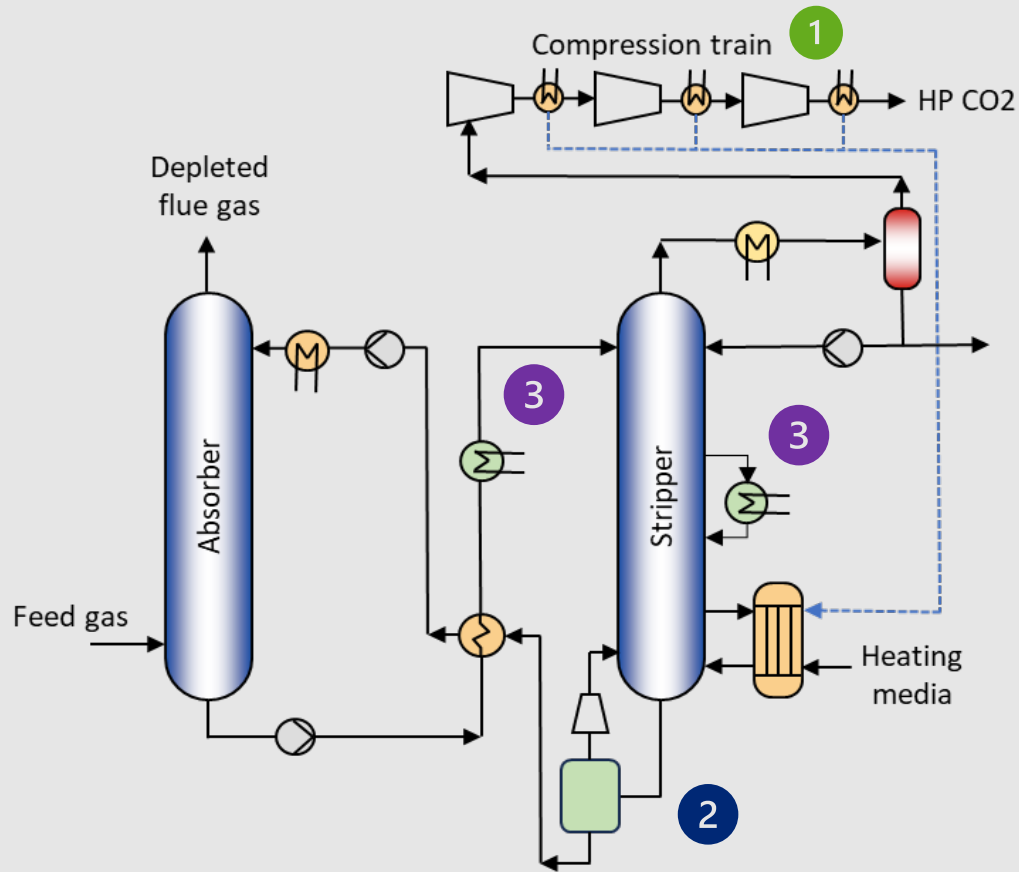


# Energy Reduction Potential

1 Compression train heat recovery

2 Lean vapor compression

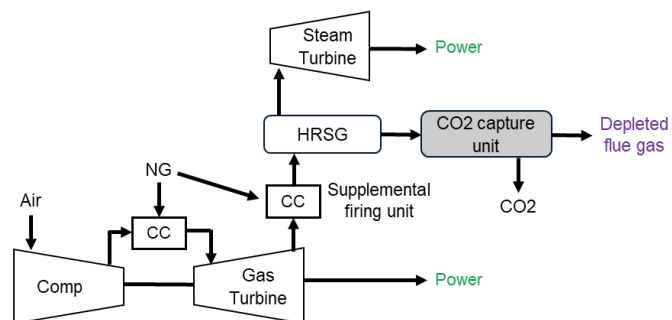
3 Waste heat integration



- Regeneration efficiency saving between 0.2 – 0.5 GJ / tonne - CO<sub>2</sub>
- Saving of 0.1 GJ / tonne of CO<sub>2</sub> in 1100 MWel plant
  - ▶ ~ 37 tonnes of LP steam / hour
  - ▶ ~ 0.5 % of electrical power plant output

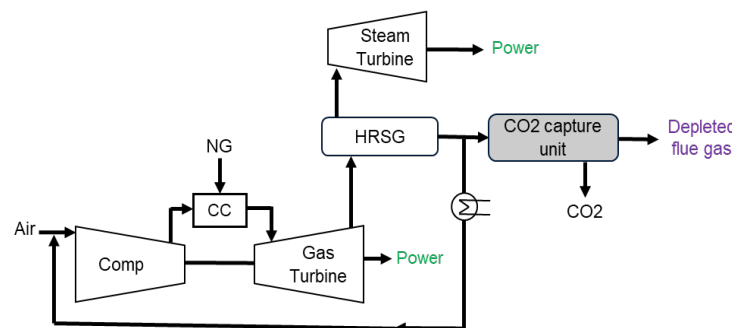
# How to Increase CO<sub>2</sub> in Flue Gas?

## Supplemental firing



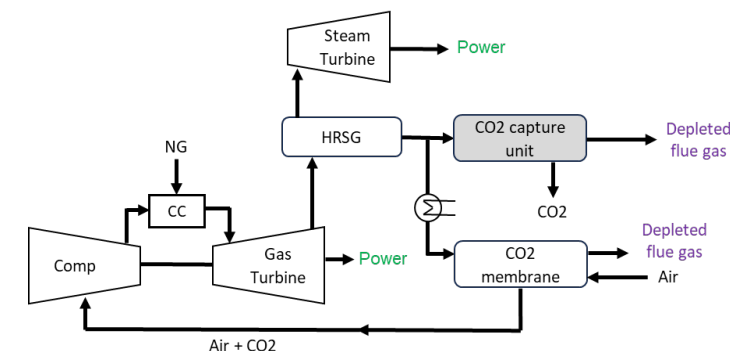
- Combustion of additional fuel at outlet of GT
- Reduces O<sub>2</sub> and increases CO<sub>2</sub> to 10 mol%
- **Challenge:** Higher T at inlet of HRSG affects material selection

## Exhaust gas recirculation (EGR)



- Recycle portion of flue gas to compressor inlet
- Reduces O<sub>2</sub> and increases CO<sub>2</sub> to 6.5 mol%, limited by 40% EGR ratio
- **Challenge:** flame stability in combustor

## Selective EGR with CO<sub>2</sub> membrane

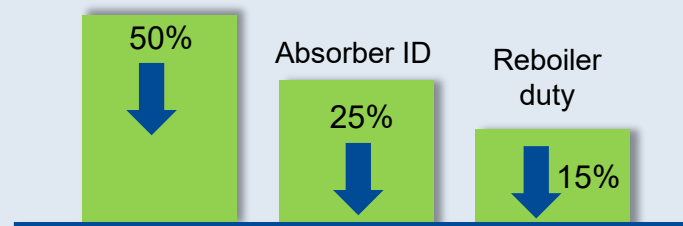


- Install CO<sub>2</sub> membrane to further concentrate CO<sub>2</sub>. Combustion air not diluted with N<sub>2</sub>
- Increases CO<sub>2</sub> to 14-18 mol% & maintain 16 mol% O<sub>2</sub> at inlet combustor
- **Challenge:** increasing operational complexity, reducing flexibility

1500 TPD CO<sub>2</sub> capture plant  
OASE blue technology  
Increases CO<sub>2</sub> from 4 to 8 mol%  
Decreases O<sub>2</sub> from 13 to 7 mol%



Solvent make up



# Key Takeaways



## Challenges

- Low CO<sub>2</sub>/O<sub>2</sub> ratio in CCGT
- Higher solvent degradation rate → OPEX
- Higher CO<sub>2</sub> capture rate requirement



## High Performance

- Significant energy saving over MEA solvent
- CO<sub>2</sub> capture rate up to 99% with CO<sub>2</sub> product purity exceeds 99%



## Optimization

- Various energy reduction options within CCS flowsheet
- Allows significant savings on CAPEX and OPEX to enable CCS implementation



We create chemistry