

# The prospects of flexible natural gas-fired CCGT with CCS within a green taxonomy

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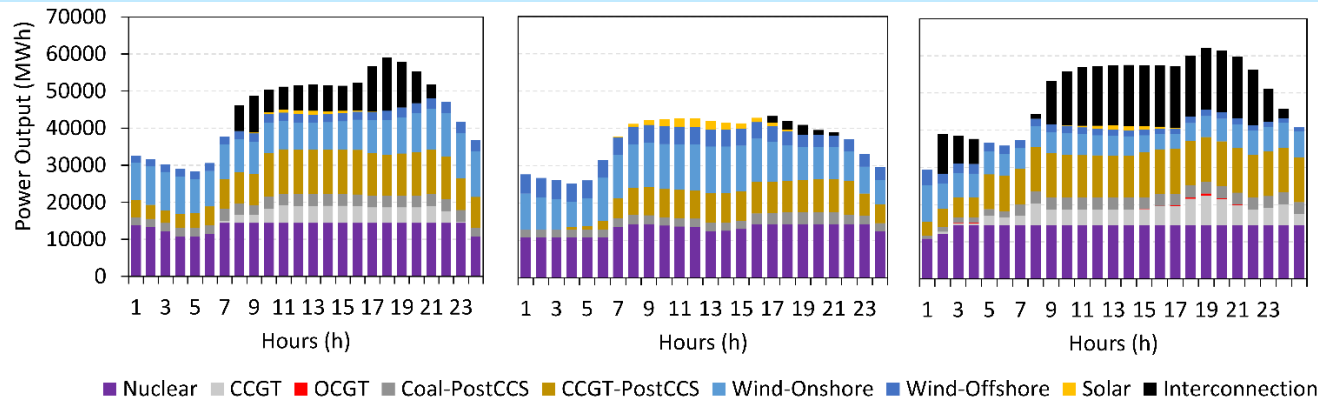
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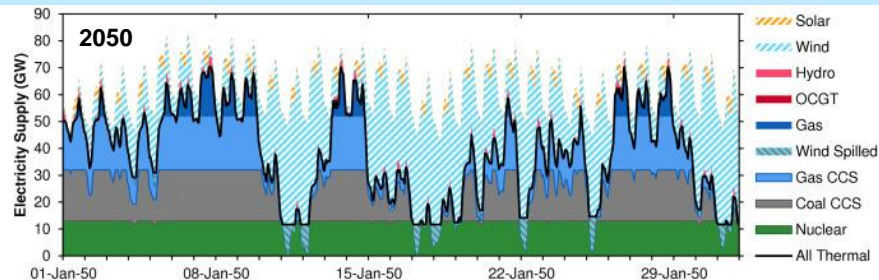
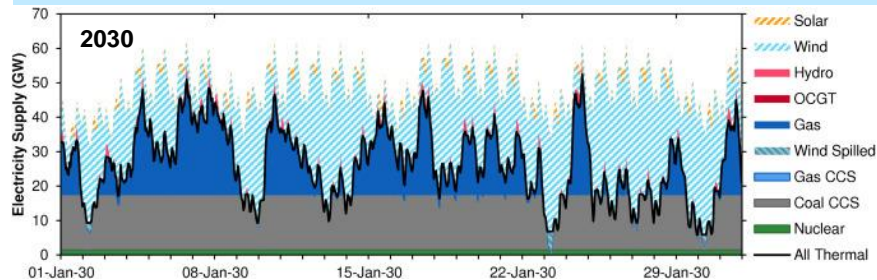
# Flexible CCS in future electricity systems

## Hourly power generation for three sample days in a 2035 UK power system

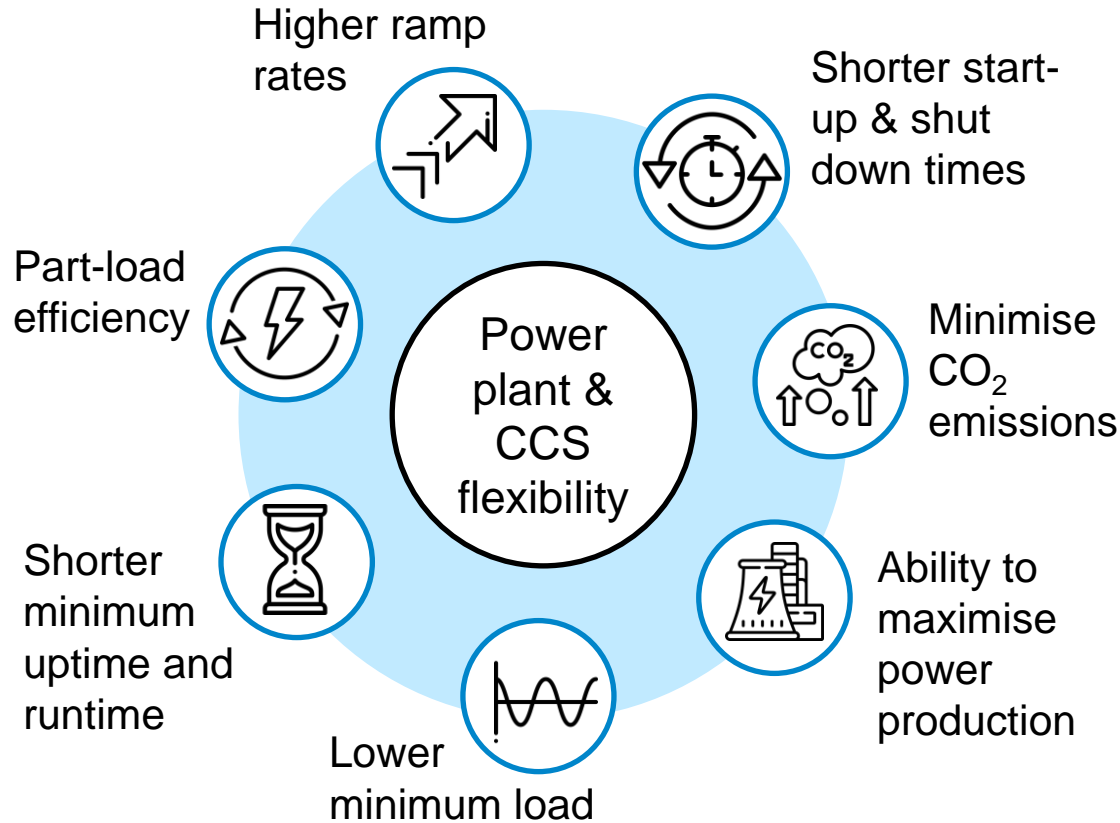
To accommodate intermittent renewables, fossil fuel power plants will need to operate flexibly.



## Electricity supply for the UK from 2030 to 2050



# Flexibility of power plants with CCS



Rise in the frequency of start-up and shut down cycles will be expected with higher levels of intermittent renewables.

If this significantly increases CO<sub>2</sub> emissions, it will undermine the value proposition of CCS.

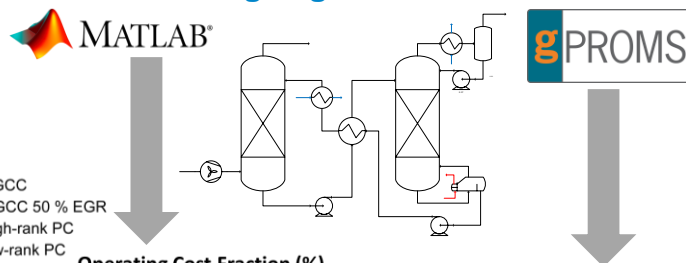
Need to ensure CO<sub>2</sub> emissions reduction requirements are being met.

# Technology development & delivery

## Process modelling

Develop understanding of the impacts on cost and technical performance

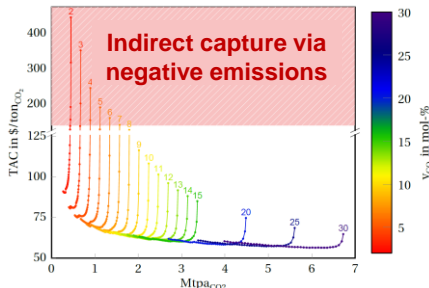
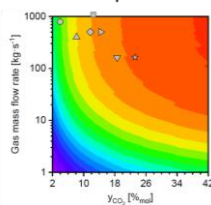
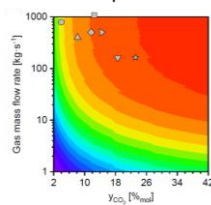
### Process modelling in gPROMS and MATLAB



Operating Cost Fraction (%)

90% capture rate

99% capture rate

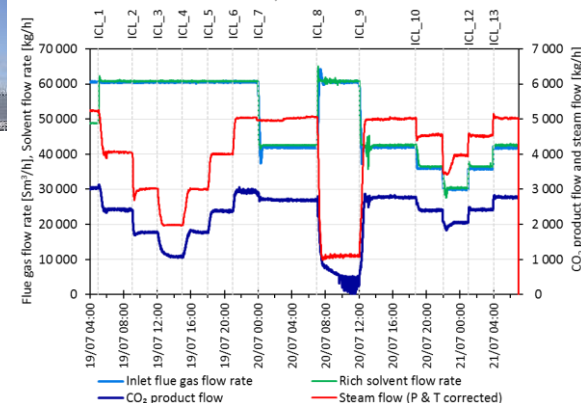
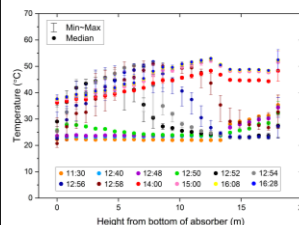


## Demonstration

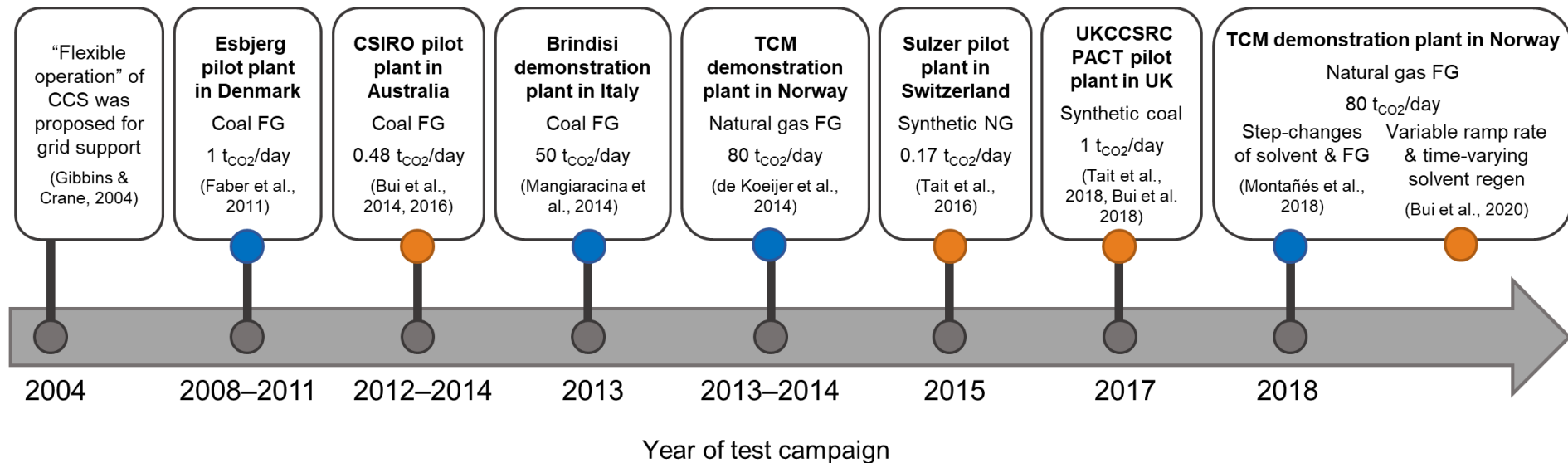
Demonstrates feasibility and develop understanding of plant operation



Operating data from demo plant



# Pilot & demonstration studies of flexible CCS operation

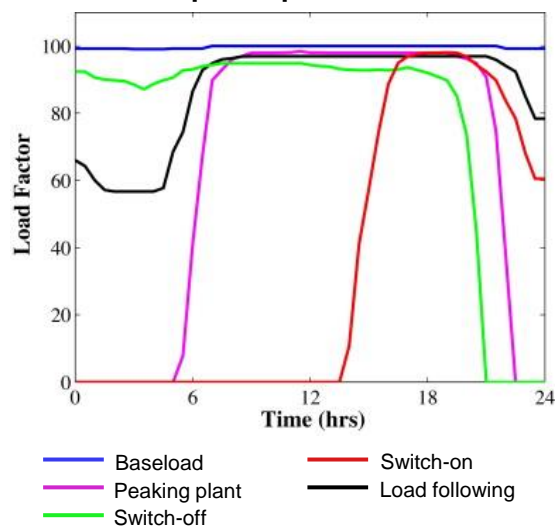


- Dynamic process data unavailable
- Dynamic process data published

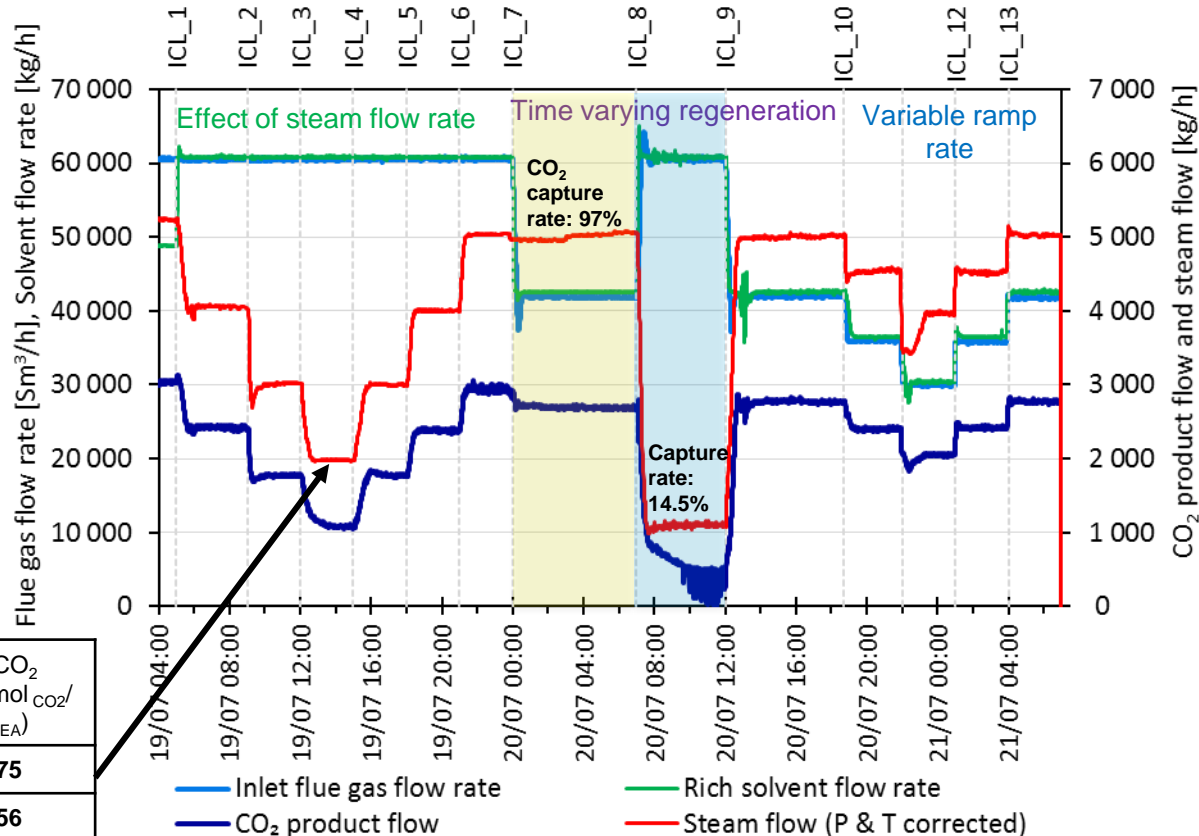
We have gained valuable operating experience at dynamic conditions.  
Dynamic operating data for model development is being made available.

# Flexibility of power plants with CCS

Typical modes of operation for fossil fuel-fired power plants in the UK



Steam flow rate (kg/h)	CO <sub>2</sub> capture rate (%)	Lean CO <sub>2</sub> loading (mol <sub>CO2</sub> /mol <sub>MEA</sub> )
2000	26.0	0.4375
5000	72.0	0.2456

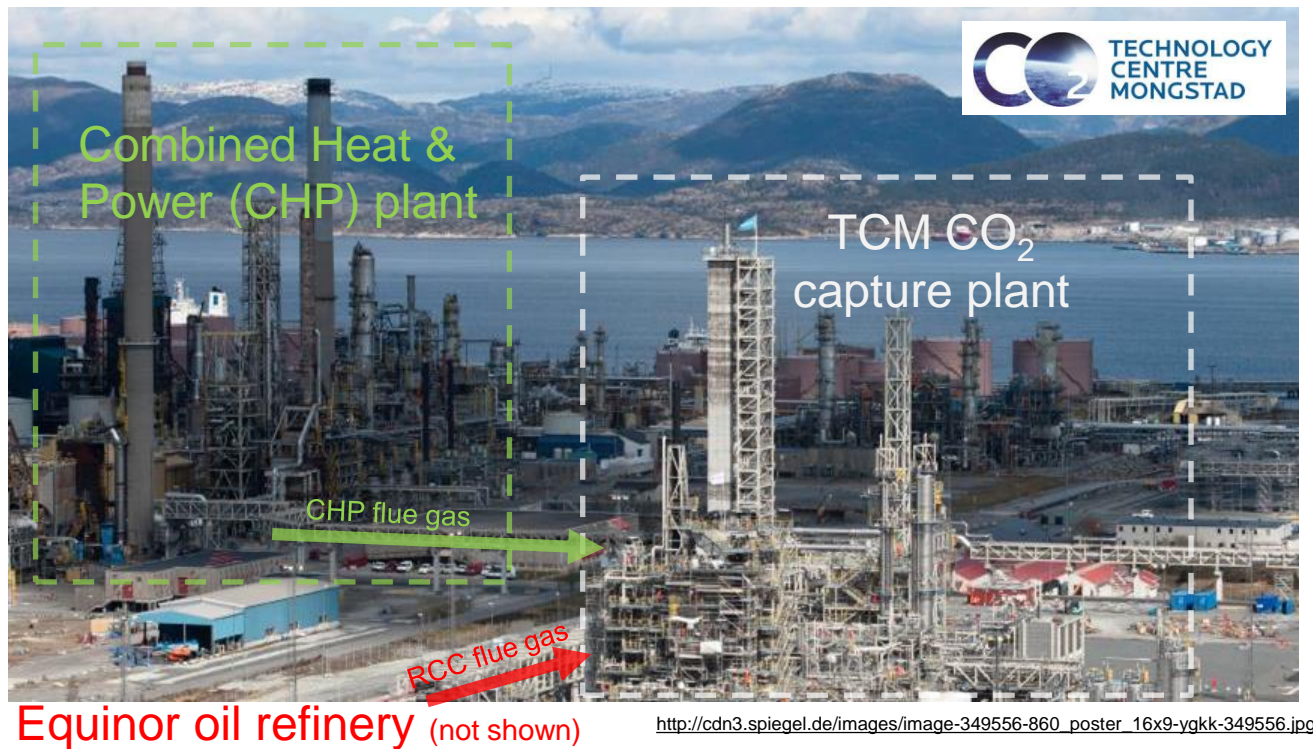




# Flexible operation of a demonstration-scale CO<sub>2</sub> capture plant

In 2020, we studied the effect of start-up & shut down on CO<sub>2</sub> emissions at TCM.

Studying the following: (i) hot vs cold start-up, (ii) timing of steam availability (conventional vs preheat vs delayed), (iii) solvent inventory capacity, (iv) start-up solvent loading/composition.



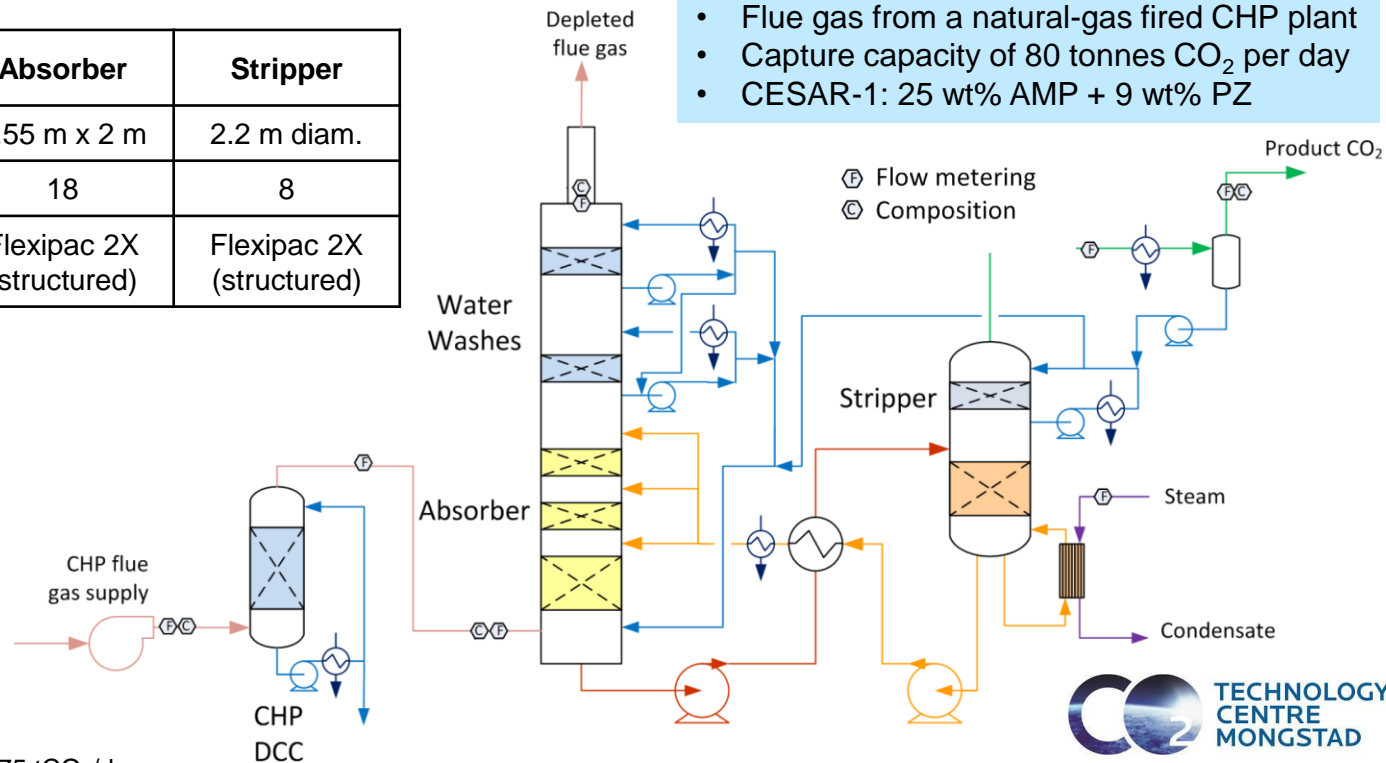
# TCM CO<sub>2</sub> capture facility, Mongstad Norway

	Absorber	Stripper
<b>Cross section dimensions</b>	3.55 m x 2 m	2.2 m diam.
<b>Packing height (m)</b>	18	8
<b>Packing type</b>	Flexipac 2X (structured)	Flexipac 2X (structured)

Flue gas component	CHP
	mole %
N <sub>2</sub>	71.6 – 78.6
CO <sub>2</sub>	3.5 – 4.3
H <sub>2</sub> O	2.5 – 6.3
O <sub>2</sub>	12.5 – 14.4
Ar	0.9 – 1.0

## Combined heat and power (CHP) mode

- Flue gas from a natural-gas fired CHP plant
- Capture capacity of 80 tonnes CO<sub>2</sub> per day
- CESAR-1: 25 wt% AMP + 9 wt% PZ

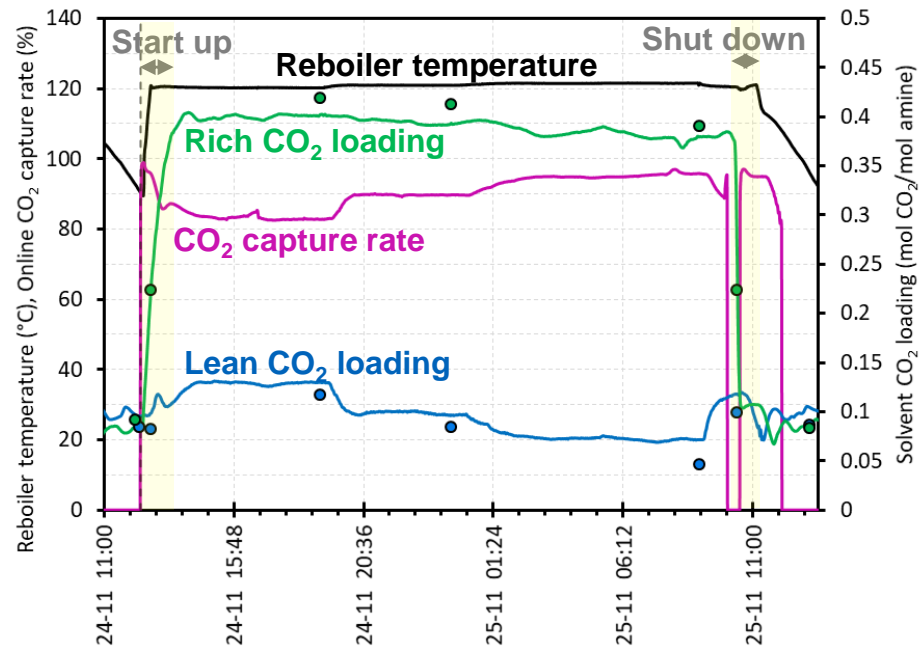
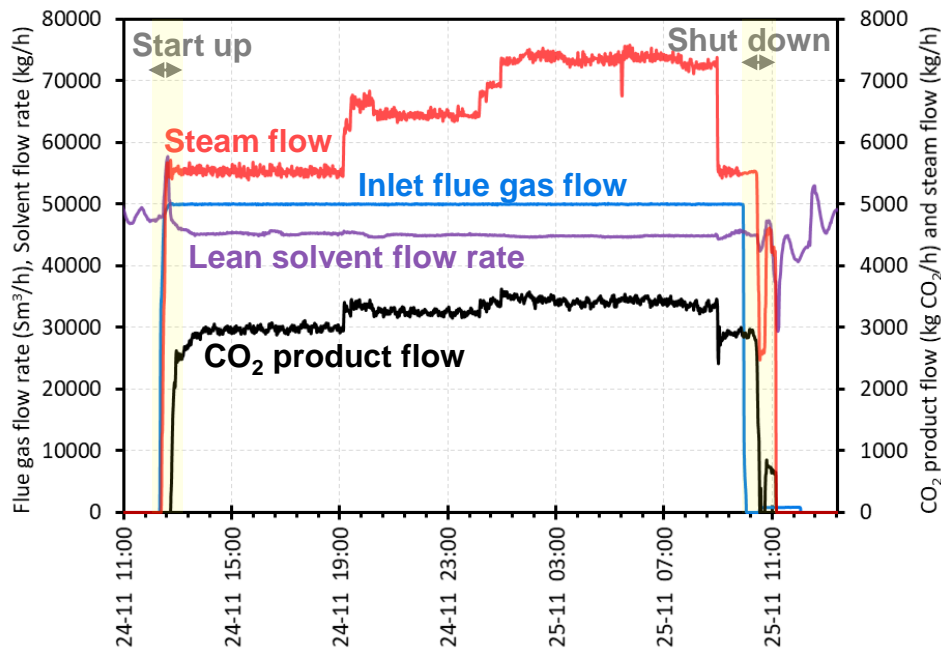


RCC mode: gas 12 mol% CO<sub>2</sub>, captures 275 tCO<sub>2</sub>/day



# Start-up and shut down tests at TCM

Hot start-up and shut down with 53 m<sup>3</sup> solvent inventory

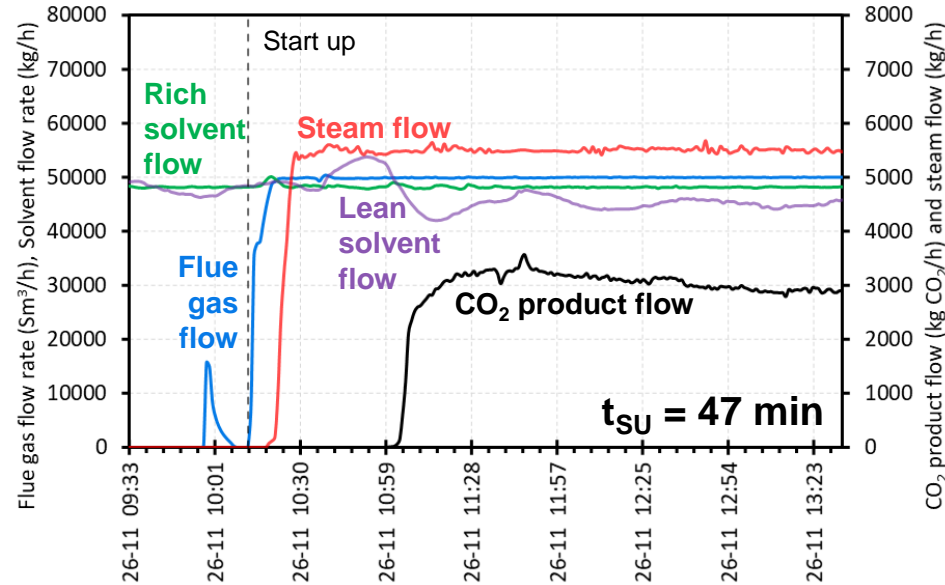


**Start up:** Flue gas flow is turned on, steam flow begins earlier, at same time, or delayed.

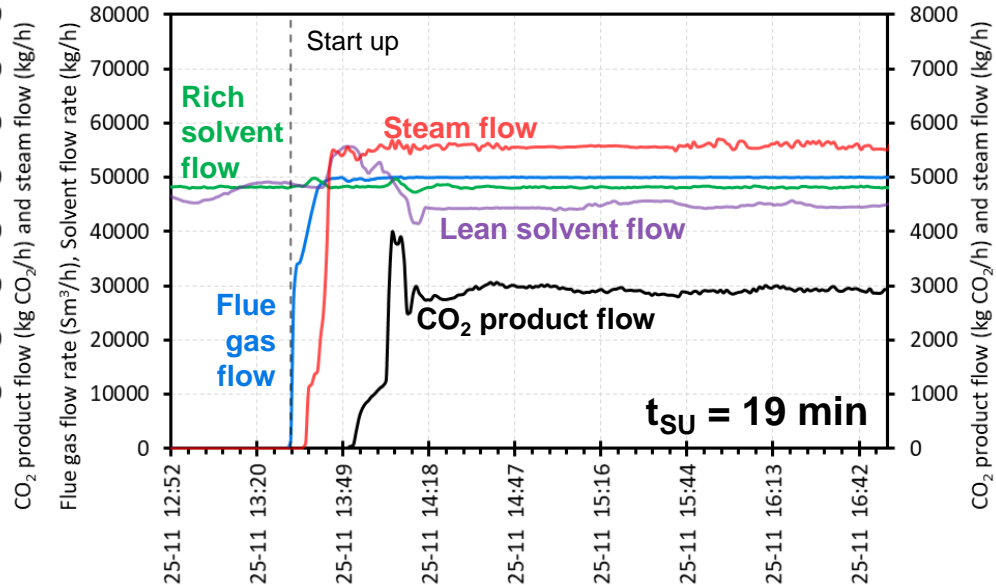
**Shut down:** Flue gas flow ramps down, steam flow rate continues until target solvent loading is achieved.

# Cold vs hot start-up

## Cold start-up with 42 m<sup>3</sup> solvent inventory



## Hot start-up with 42 m<sup>3</sup> solvent inventory

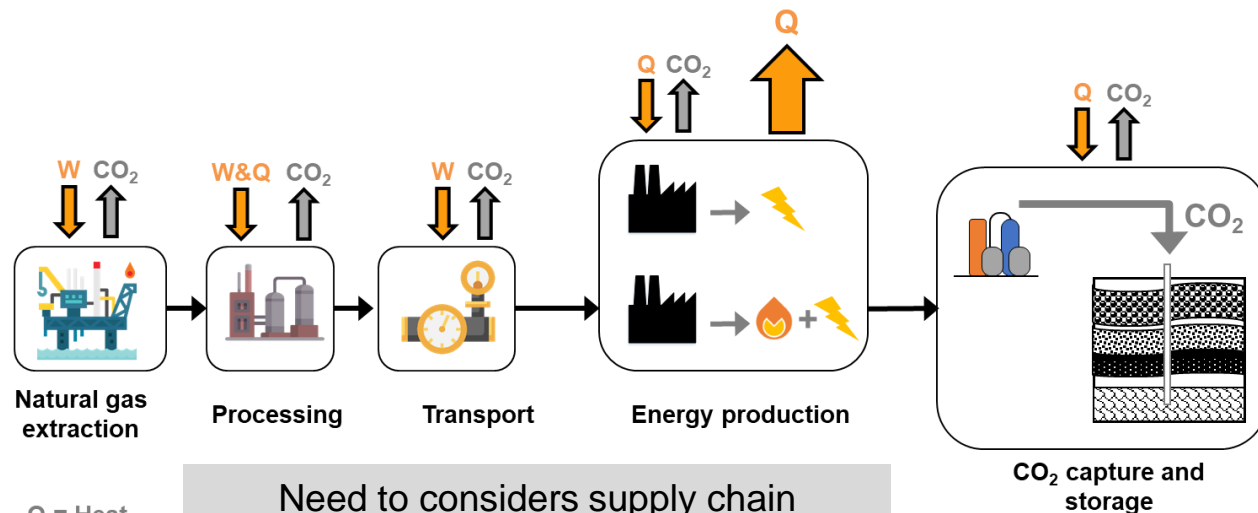


**Cold start-up:** performed after a long downtime, i.e., >8 hours, stripper cools to near ambient temperature (25 – 40 °C). The time when CO<sub>2</sub> product flow starts is  $t_{SU}$ . Test above has steam flow starting at a similar time to the flue gas flow.

**Hot start-up:** performed after a short downtime, i.e., off for <8 hours, stripper is still high temperature at 80 °C or above. Thus, hot start-ups are much quicker than cold start-ups (shorter  $t_{SU}$ ).

- High capture rates above 90% is techno-economically feasible (at steady state).
- During dynamic operation, 90% capture rate is feasible with load following regimes (e.g., ramp up/down) and hot start-up and shut down.
- During cold start-up and shut down, CO<sub>2</sub> capture rates can reduce to 50% or lower.
- Increased start-up and shut down cycles could increase CO<sub>2</sub> emissions of a CCGT significantly.

82 min start-up (SU) combined with shut down (SD)	Zero emissions intensity steam		With an NG auxiliary boiler for SUSD	
	Cumulative specific reboiler duty (MJ/kg CO <sub>2</sub> )	Cumulative CO <sub>2</sub> captured (%)	Cumulative specific reboiler duty (MJ/kg CO <sub>2</sub> )	Cumulative CO <sub>2</sub> captured (%)
Cold SU 53 m <sup>3</sup> & SD	8.15	80.0	12.42	52.5
Cold SU 42 m <sup>3</sup> & SD	8.51	66.3	13.04	43.3
Hot SU 53 m <sup>3</sup> & SD	6.06	97.3	7.26	81.2
Hot SU 42 m <sup>3</sup> & SD	5.94	96.5	6.93	82.9
Hot SU 42 m <sup>3</sup> delayed steam & SD	6.17	67.7	7.35	56.8

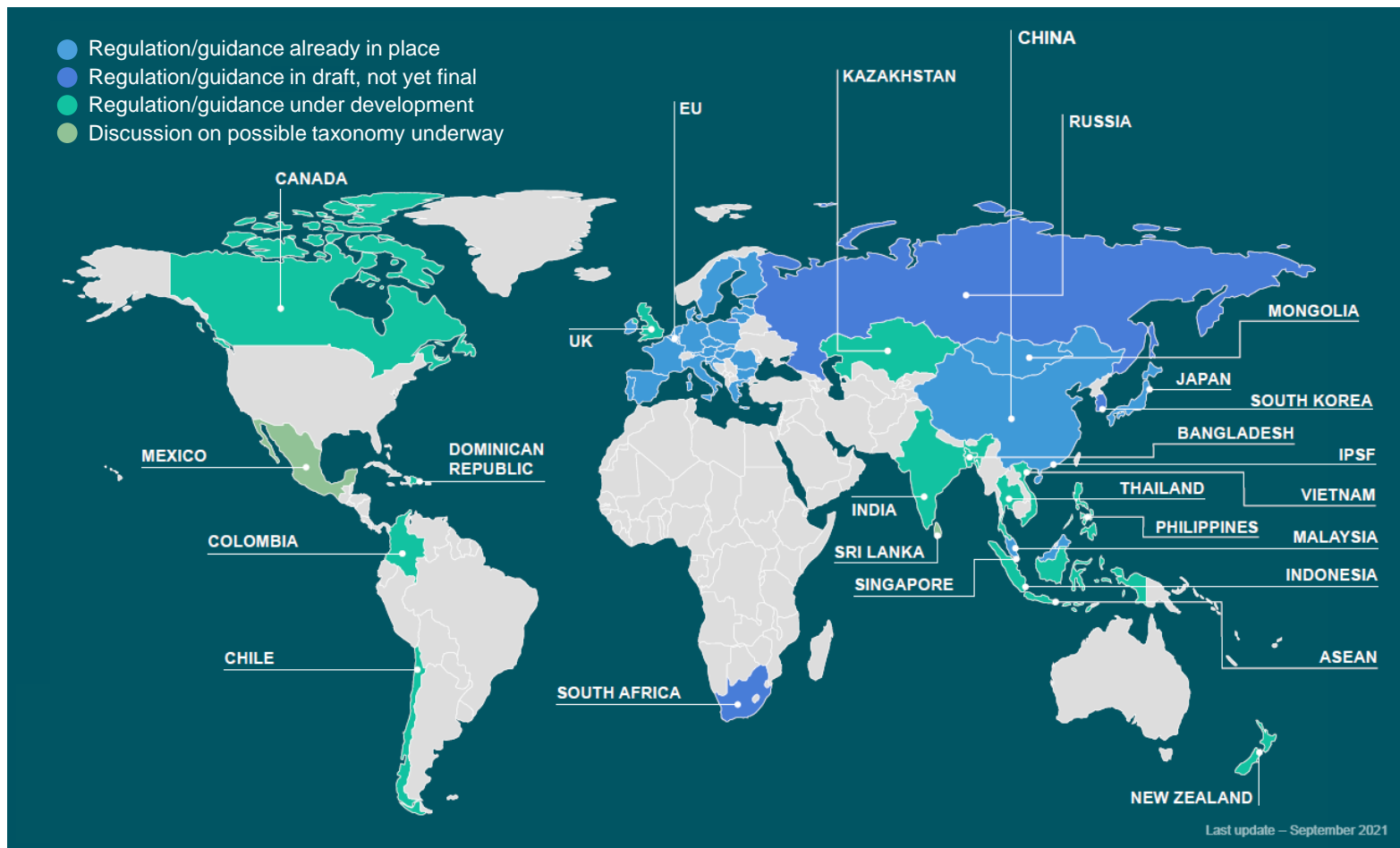


Need to consider supply chain emissions CO<sub>2</sub>eq including methane leakage

Provides financial firms guidance on which activities qualify as being “green”.

Technology-agnostic emissions threshold of 100 kg CO<sub>2</sub> eq/MWh for electricity generation, heat production and co-generation of heat and electricity.

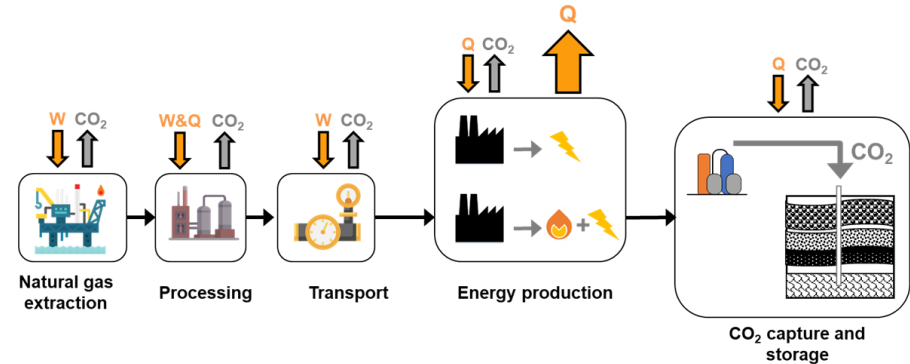
For hydrogen production, the lifecycle GHG emissions threshold needs to be lower than 3 tCO<sub>2</sub> eq/t H<sub>2</sub>, which favours green and blue hydrogen.



To determine the eligibility of a combined cycle gas turbine (CCGT) power plants within any future sustainable green taxonomy.

Evaluated the effect of the following factors on the CO<sub>2</sub> intensity of electricity generation by a CCGT power plant:

- Natural gas supply chain emissions;
- CO<sub>2</sub> capture rate;
- Switching to blue hydrogen;
- Number and type (e.g., cold vs hot) of start-up and shut down cycles.





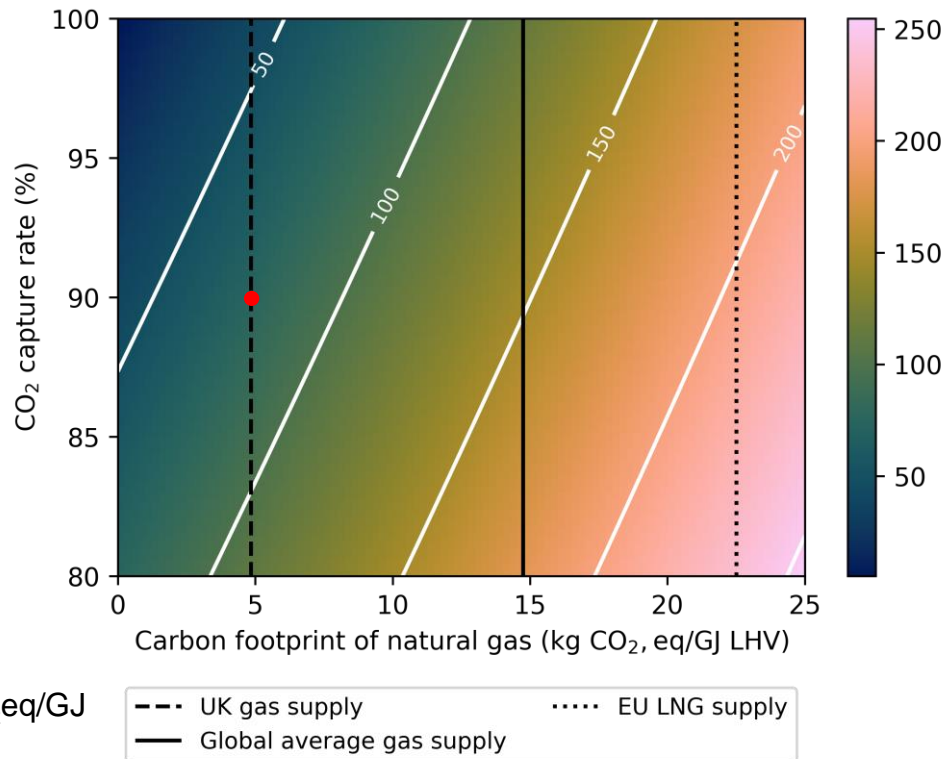
At steady state operation, a CCGT-CCS plant using UK gas would need to capture 82.5% of the CO<sub>2</sub> to meet the 100 kg CO<sub>2</sub>eq/MWh<sub>el</sub> criteria.

The steady state CO<sub>2</sub> intensity of a CCGT-CCS using UK gas with a 90% capture rate is **75.2 kg CO<sub>2</sub>eq/MWh<sub>el</sub>**.

UK supply chain carbon footprint of natural gas = 4.9 kg CO<sub>2</sub>eq/GJ LHV (Wernet et al. 2019)

## Natural gas CCGT-CCS

Carbon footprint of CCGT-CCS (kg CO<sub>2</sub>, eq/MWh)

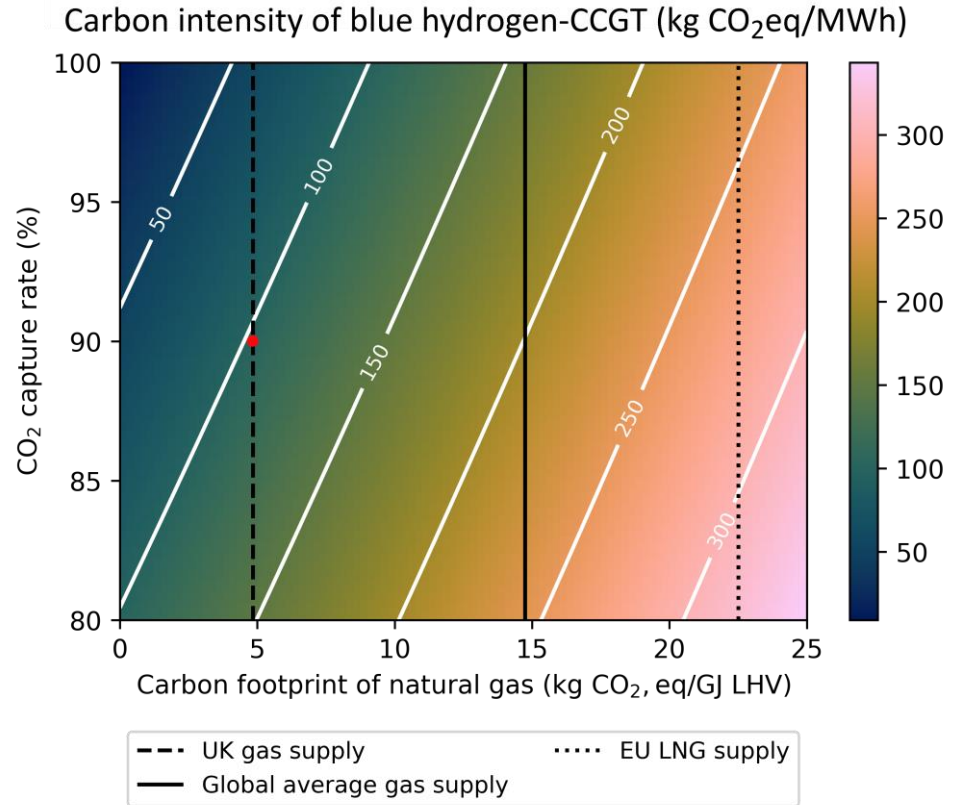


Using UK natural gas for SMR retrofitted with CCS and capturing 90% CO<sub>2</sub> to produce hydrogen for a steady state CCGT results in a CO<sub>2</sub> intensity of **103 kg CO<sub>2</sub> eq/MWh<sub>el</sub>**.

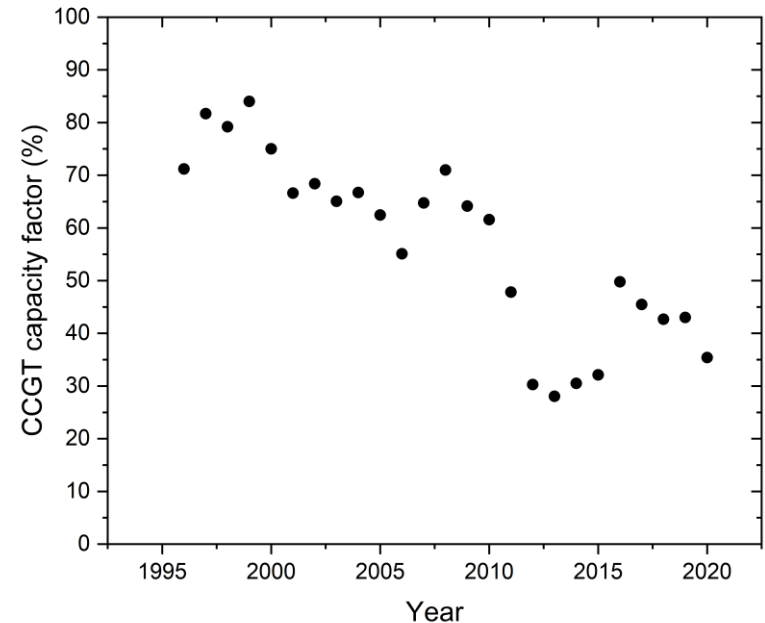
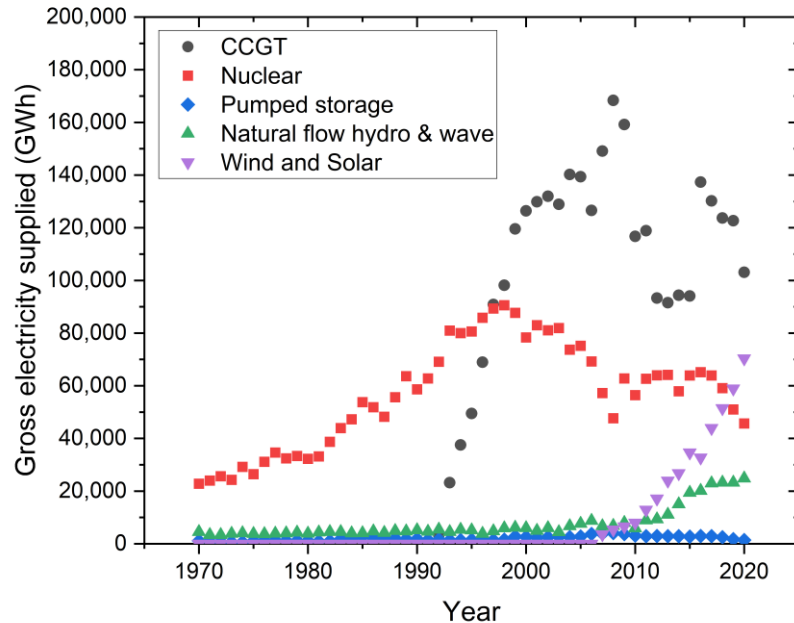
To satisfy the green taxonomy, need to use: (i) >91% CO<sub>2</sub> capture rate, (ii) reduce natural gas supply chain emissions, or (iii) use green hydrogen.

Assuming a CO<sub>2</sub> capture rate of 95% could achieve 80 kg CO<sub>2</sub> eq/MWh<sub>el</sub> with a blue hydrogen-CCGT.

## Hydrogen CCGT-CCS

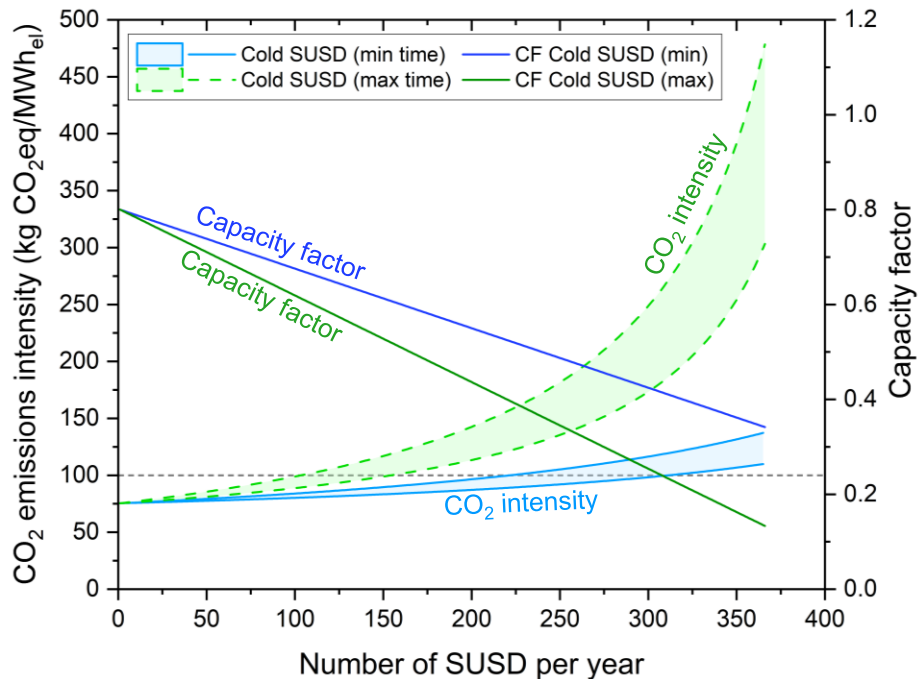
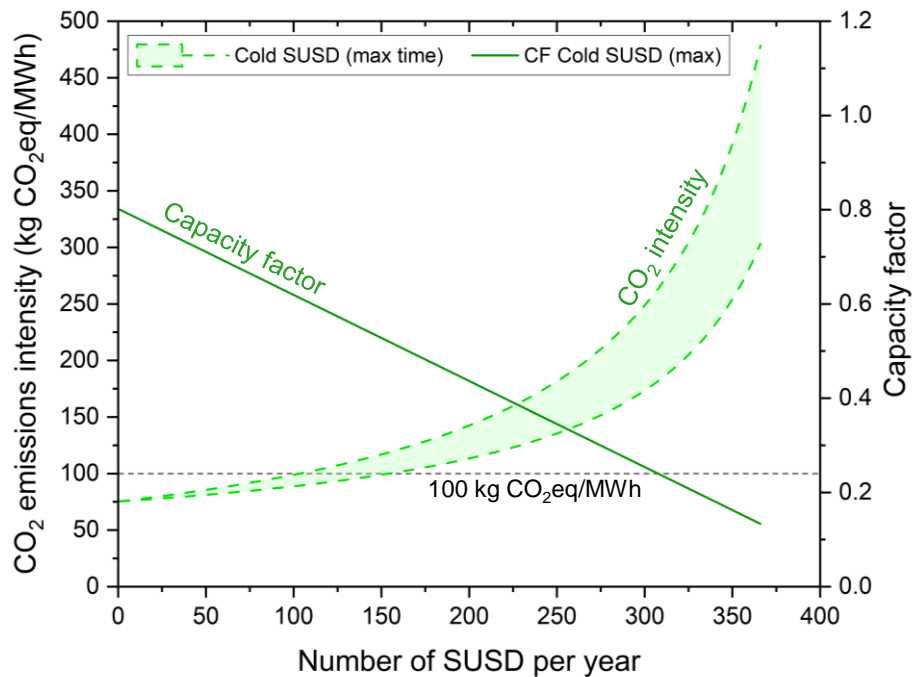


# Gross electricity supply and average annual capacity factor of UK gas-CCGT plants



# Effect of start-up & shut down on CCGT-CCS emissions

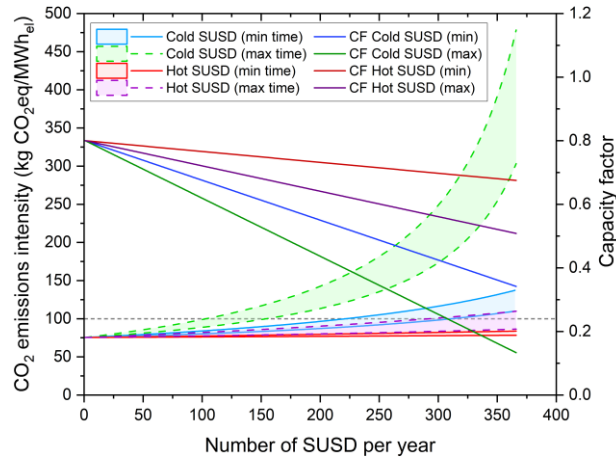
The EU taxonomy proposes an overarching, technology-agnostic emissions threshold of 100 kg CO<sub>2</sub> eq/MWh for electricity generation, heat production and co-generation of heat and electricity.



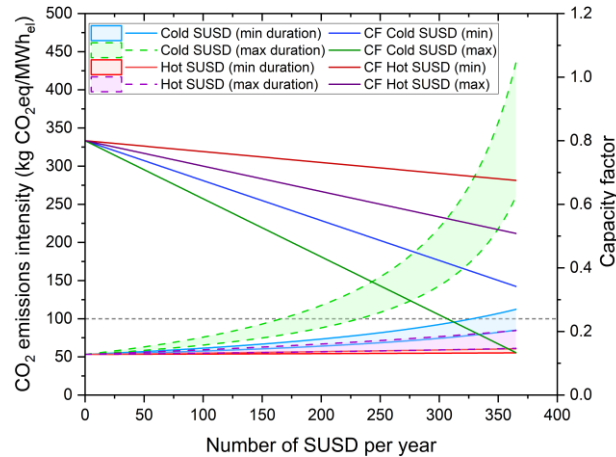
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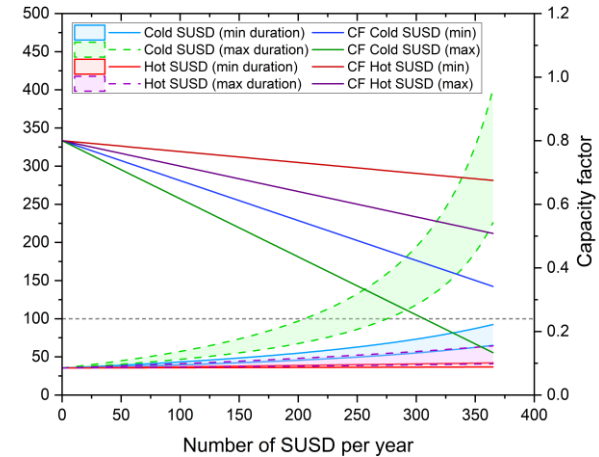
**90% capture rate**



**95% capture rate**



**99% capture rate**



As the number of SUSD cycles increases, the CO<sub>2</sub> emissions intensity becomes increasingly higher, and the capacity factor reduces. Higher CO<sub>2</sub> capture rates ensures that taxonomy emissions threshold can be met during flexible operation.

# NG CCGT-CCS: Green taxonomy

To remain below 100 kg CO<sub>2</sub>eq/MWh<sub>el</sub>

	Number of start-up and shut down cycles	
<b>90% capture @ steady state</b>	NG auxiliary boiler	Zero emissions aux boiler
Cold SUSD (min duration)	221	311
Cold SUSD (max duration)	102	153
Hot SUSD (min duration)	No limit	No limit
Hot SUSD (max duration)	291	No limit

	Number of start-up and shut down cycles	
<b>95% capture @ steady state</b>	NG auxiliary boiler	Zero emissions aux boiler
Cold SUSD (min duration)	328	No limit
Cold SUSD (max duration)	166	232
Hot SUSD (min duration)	No limit	No limit
Hot SUSD (max duration)	No limit	No limit



# Conclusions

With higher penetration of renewable energy, thermal power plants with CCS could have an important role in providing low carbon, dispatchable electricity.

Understanding the potential impact of key process decisions on the prospects of existing and future fossil fuel-based power generation under a green taxonomy will be essential to ensure a cost-effective transition to net zero.

For NG CCGT-CCS, key considerations include reducing methane leakage, high CO<sub>2</sub> capture rates, and minimising the impacts of start-up and shut down cycles performed by the CCGT-CCS plant.

The main advantage of hydrogen-fired CCGT is that SUSD and highly flexible operation will not increase the CO<sub>2</sub> emissions intensity of the electricity. However, the hydrogen fuel needs to be highly carbon efficient to meet the EU taxonomy.

In order for natural gas to play an enduring role in the transition towards net zero, managing GHG emissions from both the upstream natural gas supply chain and the conversion facility is key.

The ability to maximise the CO<sub>2</sub> capture during start-up and shut down reduces residual CO<sub>2</sub> emissions, thus easing the need for CO<sub>2</sub> removal offsets, e.g., from bioenergy with CCS or direct air capture technologies.

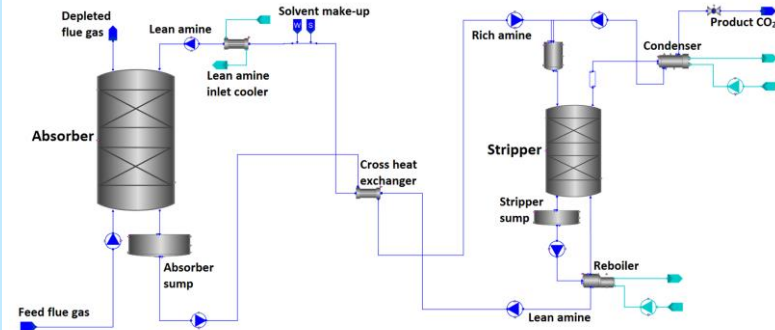
# Conclusions and future work

These learnings will help improve the performance of flexible operation and SUSD strategies in CO<sub>2</sub> capture plants.

The data from this study will help in the development more robust process control systems, as well as improve the description of flexible and dynamic operation in process & systems models.

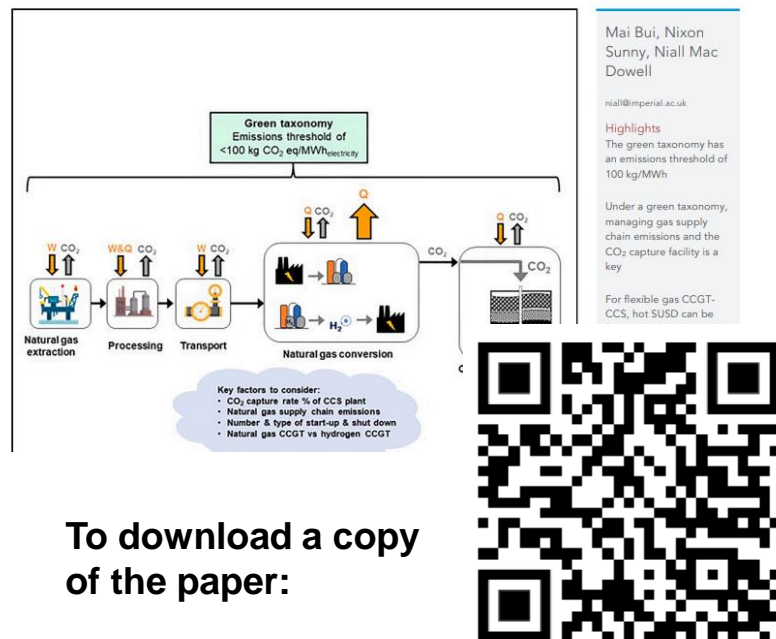
## Future work:

- Investigate the impact of different process configurations and process control systems that could improve plant flexibility and SUSD performance, e.g., via process modelling.
- Effect of different solvent types on CO<sub>2</sub> capture plant flexibility and SUSD performance.
- Study dynamic interactions between the power plant and CCS process, also upstream/downstream effects.
- Techno-economic analysis to understand the cost implications of different SUSD strategies.
- Understand the impact of SUSD cycles at a systems scale, i.e., effect on ability to reach net zero.



## Article

## The prospects of flexible natural gas-fired CCGT within a green taxonomy



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#### Highlights

The green taxonomy has an emissions threshold of 100 kg/MWh

Under a green taxonomy, managing gas supply chain emissions and the CO<sub>2</sub> capture facility is a key

For flexible gas CCGT-CCS, hot SUSD can be

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IEAGHG Technical Report  
2022-08  
August 2022

# Start-up and Shutdown Protocol for Natural Gas-fired Power Stations with CO<sub>2</sub> Capture

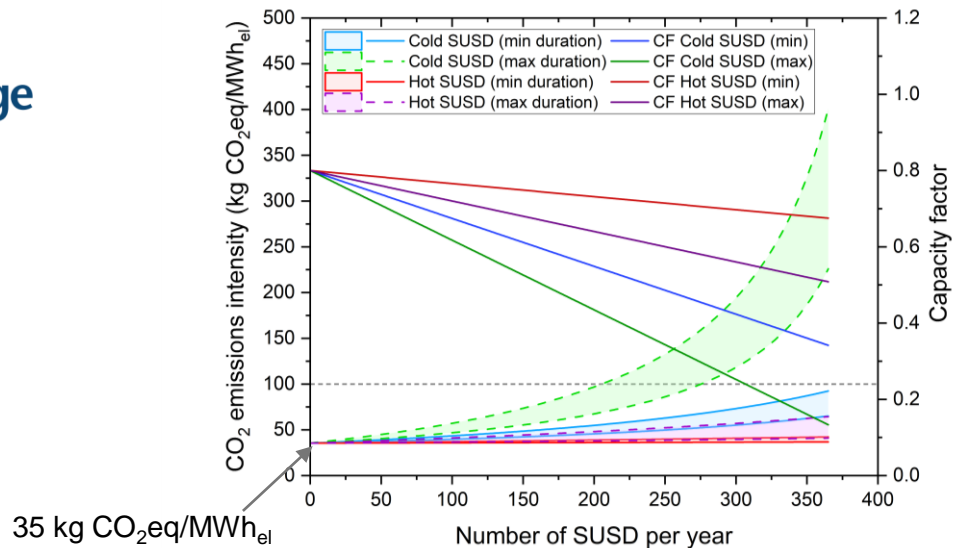
# Appendix

# Flexibility Requirements of gas power plants

		<b>OCGT</b>	<b>Recips</b>	<b>CCGT</b>
Efficiency	%	<40%	<40%	<63%
Plant size	MW	1 – 299	5 – 49	500 to 2500
Location / scale		Utility or industrial, centralised or decentralised	Industrial	Centralised / utility
Operating mode		Peaking	Peaking	Baseload / shifting
Number of starts	#	350 – 700	350 – 700	50 – 300
Hours per year	hrs/yr	500 – 2000	500 – 2000	4000 – 8500
Start time to min load	mins	5 – 10	3 – 4	20 – 90
Start time to max load	mins	20 – 30	6 – 10	60 – 180
CCS connection				
Plant retrofit		☹	☹	☺
Plant new build		☺	☺	☺



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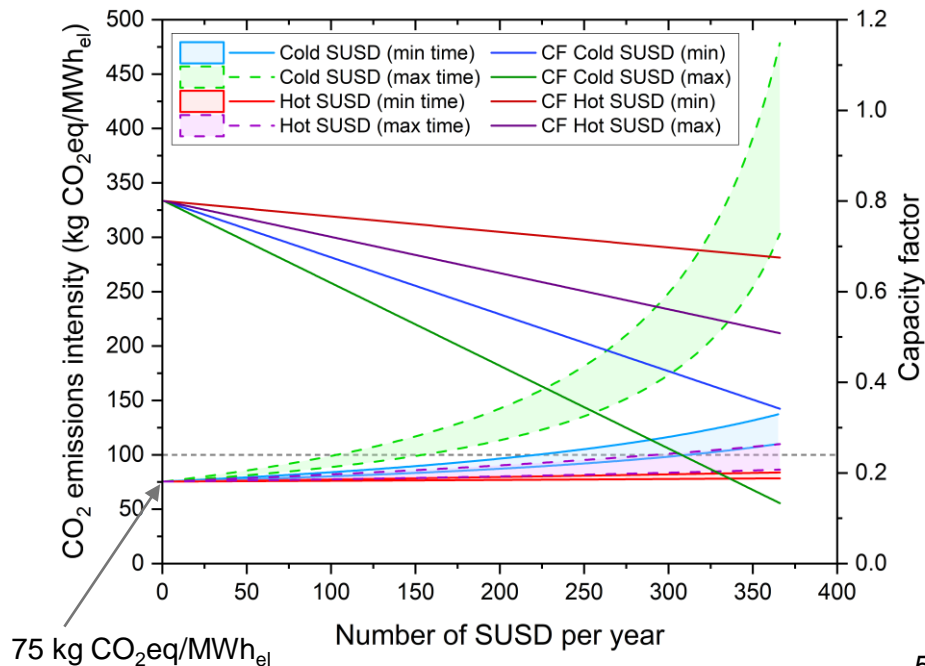


	Number of start-up and shut down cycles	
99% capture @ steady state	NG auxiliary boiler	Zero emissions aux boiler
Cold SUSD (min duration)	No limit	No limit
Cold SUSD (max duration)	205	275
Hot SUSD (min duration)	No limit	No limit
Hot SUSD (max duration)	No limit	No limit

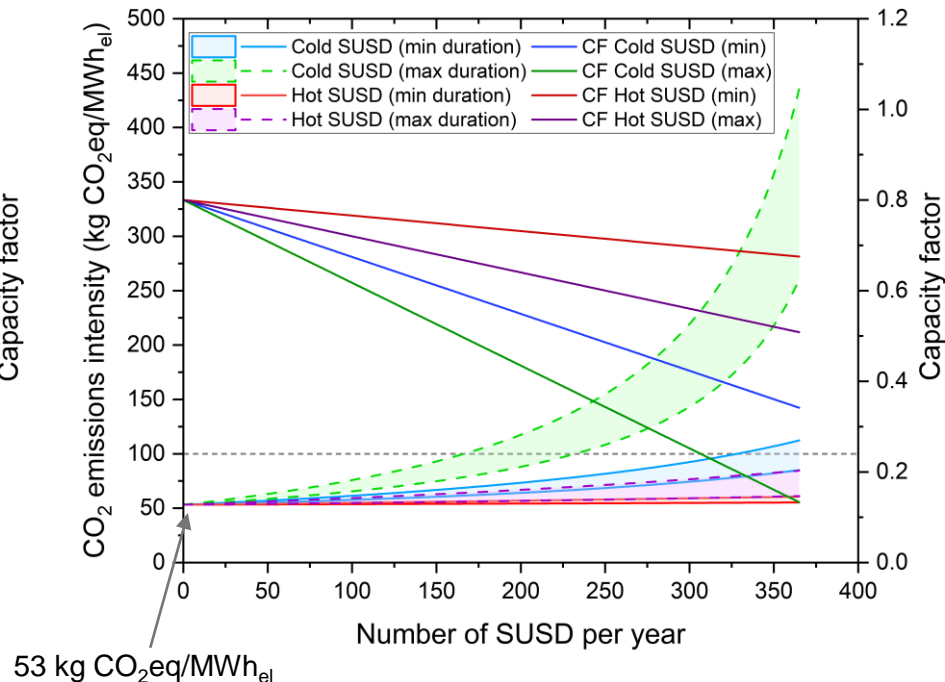


# CCGT-CCS: Effect of start-up & shut downs

## 90% capture during steady state periods



## 95% capture during steady state periods



# Characteristics of start-up and shut down types

Start-up & shut down type	Duration of one start-up & shut down cycle (h)	Downtime (h)	Cumulative CO <sub>2</sub> capture rate with zero CO <sub>2</sub> intensity auxiliary boiler (%)	Cumulative CO <sub>2</sub> capture rate, accounts for NG CO <sub>2</sub> intensity of auxiliary boiler (%)	Duration of time using auxiliary boiler for SUSP (h)
Cold start-up + shut down (Min time)	3	8	73.15	47.9	2
Cold start-up + shut down (Max time)	8	8	73.15	47.9	5
Hot start-up + shut down (Min time)	2	1	96.9	82.05	1.33
Hot start-up + shut down (Max time)	6	1	96.9	82.05	4.33

- Provides financial firms guidance on which activities qualify as being “green”.
- It is a common classification framework, provides a list of economic activities that will contribute to climate change mitigation and minimise environmental harm.
- In the EU, the green taxonomy proposes an overarching, technology-agnostic emissions threshold of 100 kg CO<sub>2</sub> eq/MWh for electricity generation, heat production and co-generation of heat and electricity.
- For hydrogen production, the lifecycle GHG emissions threshold needs to be lower than 3 tCO<sub>2</sub> eq/t H<sub>2</sub>, which favours green and blue hydrogen.
- Unabated fossil fuel-fired power plant (i.e., without CCS) will not meet the required carbon emission threshold.