



KTH Industrial Engineering  
and Management

# Combined Cycle Gas Turbines as an Energy Storage Solution in a Hydrogen Economy

*Björn Laumert – KTH*

*J. Garcia – KTH*

*R. Guédez – KTH*

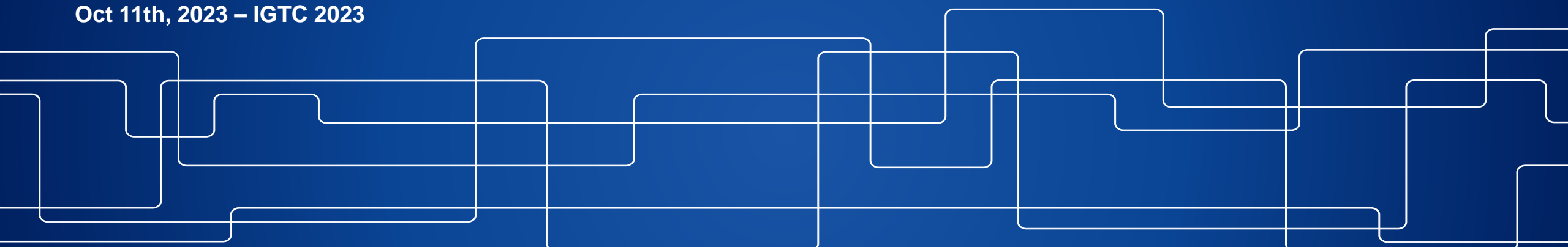


**IGTC**  
International  
Gas Turbine Conference



**ETN**  
Global

Oct 11th, 2023 – IGTC 2023



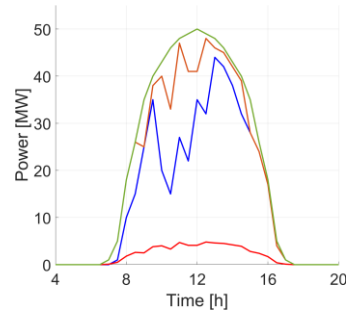
# Background / Motivation

Increased share of renewables in the energy sector



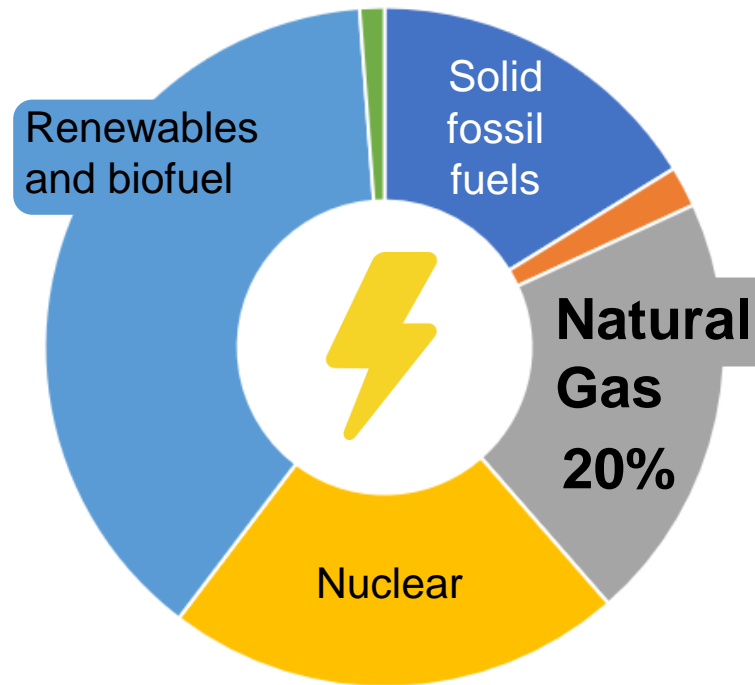
Wind and Solar

- No CO<sub>2</sub> emissions
- Competitive electricity prices
- Intermittent, non-dispatchable
- **Surplus electricity**



Fuel dependency / imports

Electricity production by fuel in EU 2022



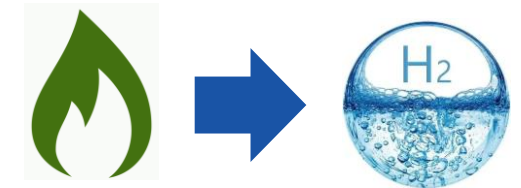
In 2021, the EU imported 83% of its natural gas consumption.

Need for:

- Energy storage



- Fuel transition

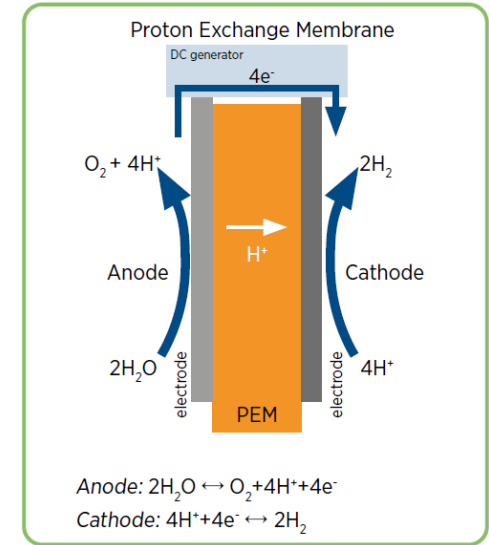
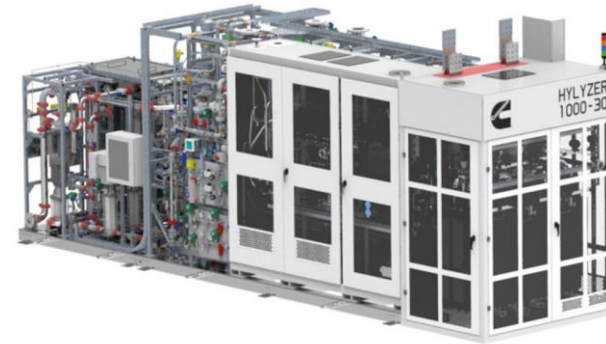


## Power-H<sub>2</sub>-Power

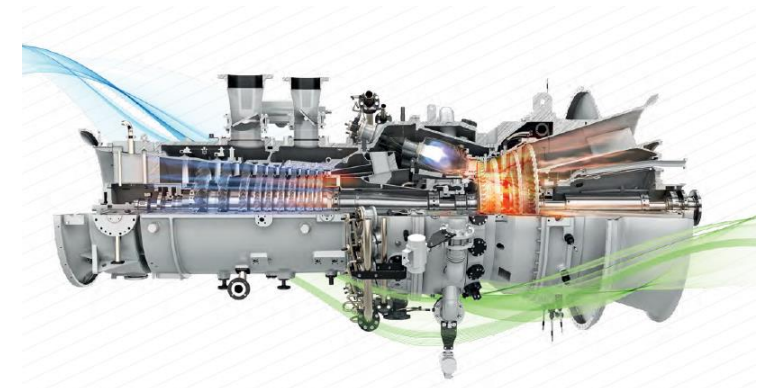
# Power to Hydrogen to Power

- PEM Electrolysers:
  - $2H_2O + Energy \rightarrow 2H_2 + O_2$
  - < 70 bar – 50-80 °C
  - 51-55 kWh/Kg – ≈ 63% (LHV)
  - Stack lifetime 80.000 hours
  - Load levelling
  - Avoid shut-downs / start-ups
  
- Gas Turbines:
  - <10% H<sub>2</sub> vol → Control / software
  - 10-30% H<sub>2</sub> vol → Materials, comb chamber
  - >30% H<sub>2</sub> vol → Intervention in GT and ST

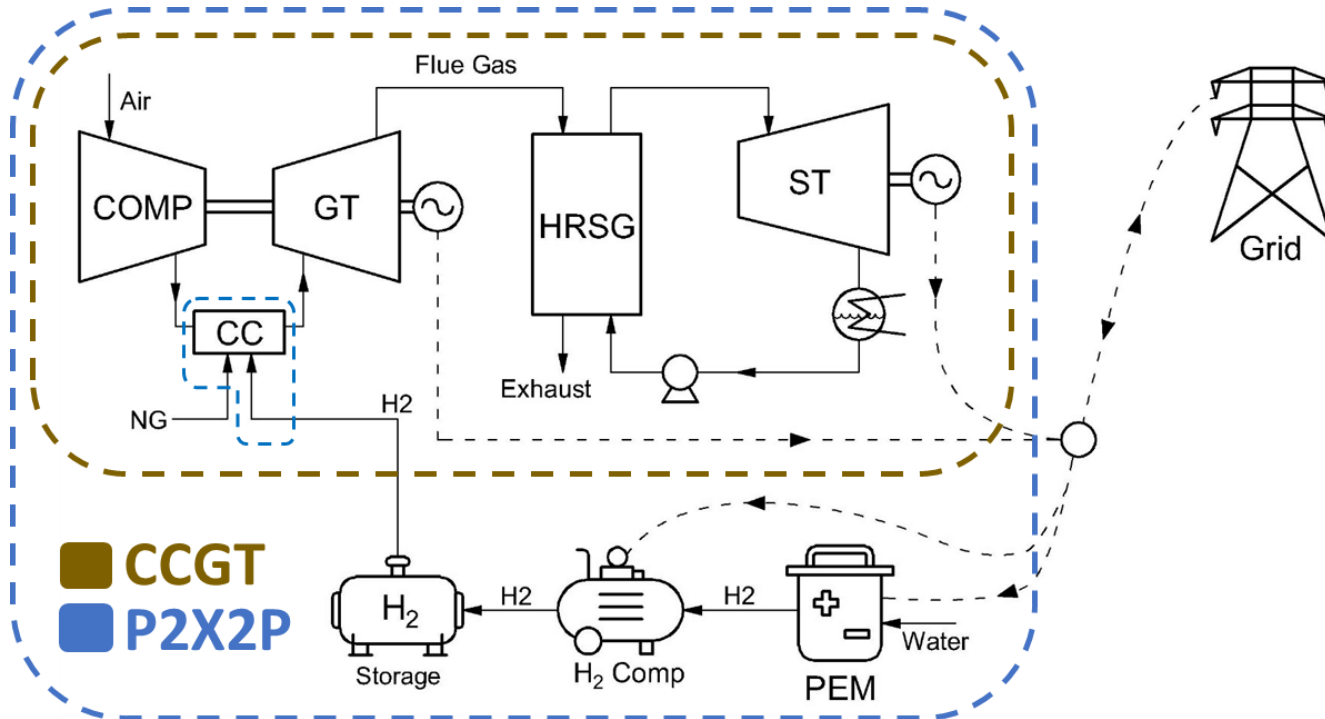
PEM Electrolysers



Hydrogen gas turbines



# Proposed layout

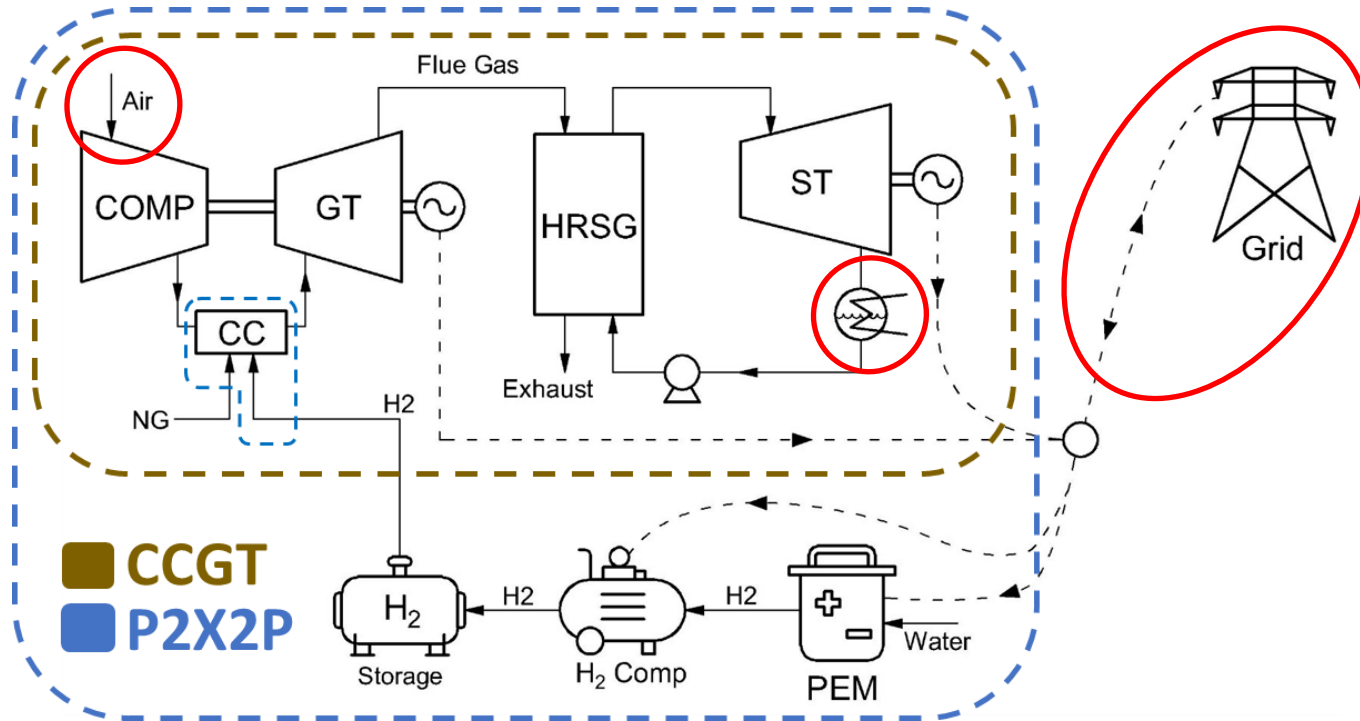


## Integration of P2X2P for:

- Energy arbitrage:  
Producing  $H_2$  during off-peak periods or high RES
- Less  $CO_2$  emissions:  
Burning alternative fossil-free fuels
- Load levelling, avoid shut-down / start-up, increased efficiency

## Techno-economic analysis

# Conditions / assumptions – Boundary conditions



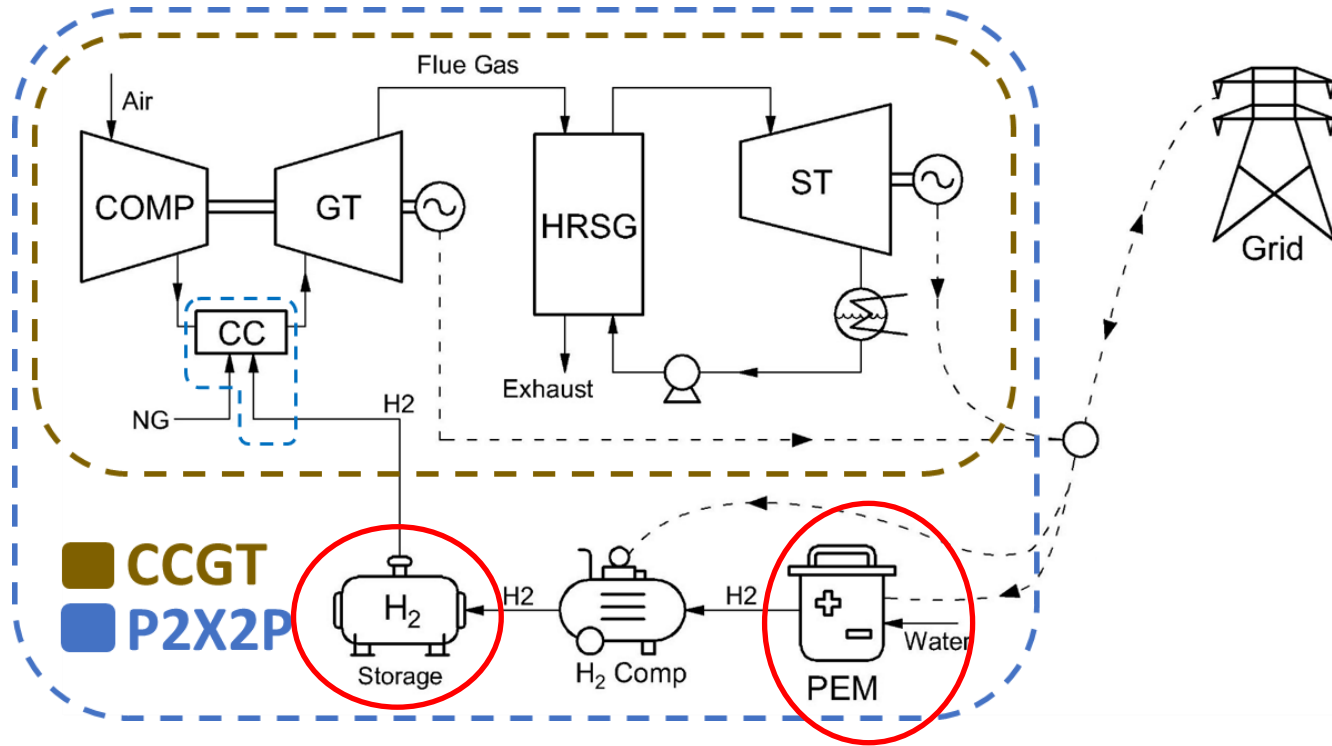
## Electric power generation

- Mid-merit or peaker
- Maximum power transfer

## Ambient conditions

- Lisbon, Portugal 2022
- Hourly values of:
  - Temperature
  - Pressure

# Conditions / assumptions – Components sizes



## Storage size

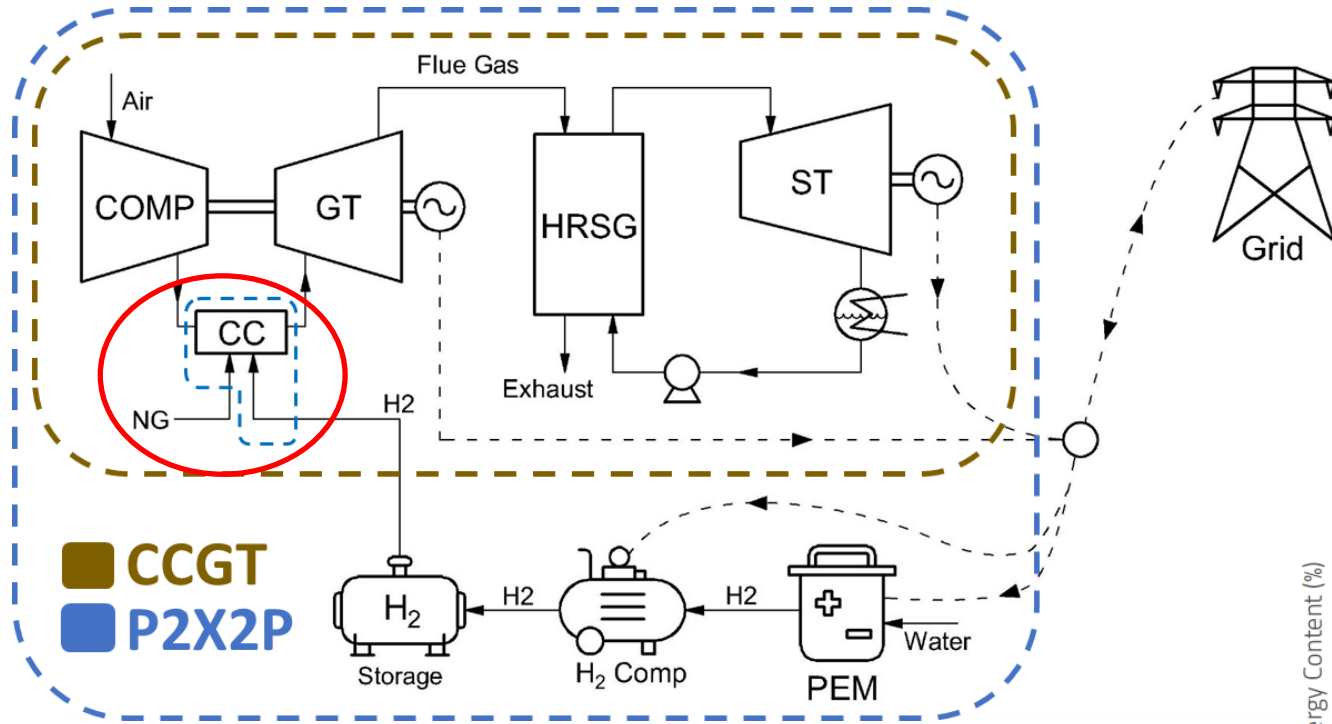
- From 0 to 24 hours of H<sub>2</sub> production

## Electrolyser size

- Relative to CCGT installed capacity
- From 0 to 1

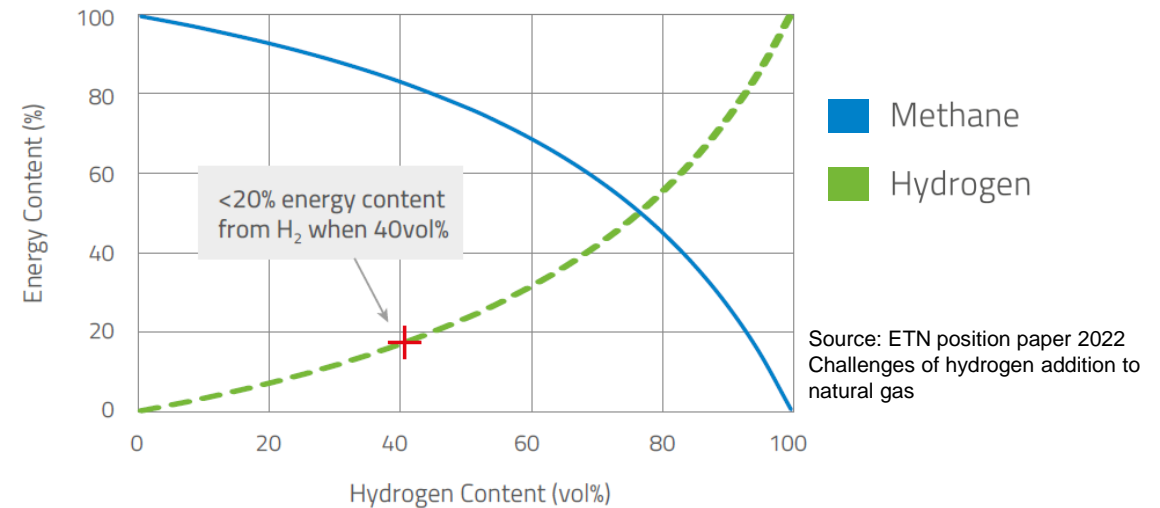
$$PEM_{size}^{rel} = \frac{PEM_{cap} [MW_e]}{CCGT_{cap} [MW_e]}$$

# Conditions / assumptions – H<sub>2</sub> mix in fuel



## Maximum H<sub>2</sub> mix in fuel

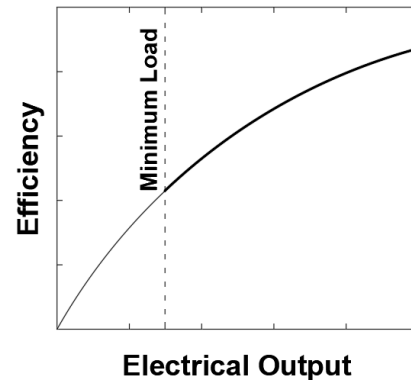
Volume	Energy	Investment
10 %	3 %	5 k€/MW <sub>el</sub>
30 %	11 %	21 k€/MW <sub>el</sub>
100 %	100 %	51 k€/MW <sub>el</sub>



# The Model: Components and costs

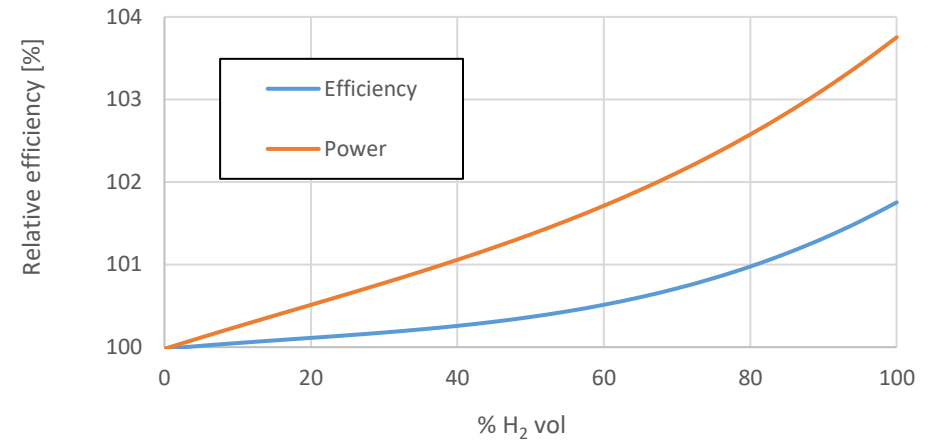
## CCGT performance

- Fixed and variable heat rate model:
  - Efficiency at part load
  - Ambient temp. and pressure
  - Saves computational time



## H<sub>2</sub> combustion in GT

Impact of H<sub>2</sub> in combustion



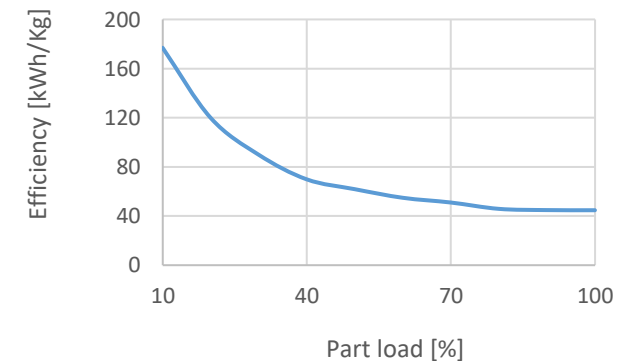
## Costs functions

$$C_{PEM} = C_{PEM}^{Ref} \cdot \left( \frac{P_{PEM,Des}}{P_{PEM,Ref}} \right)^{\alpha_{PEM}}$$

## PEM electrolyser

- Cell, stack, system level
- Validated with reference models and industrial partners
- Simplified to correlations

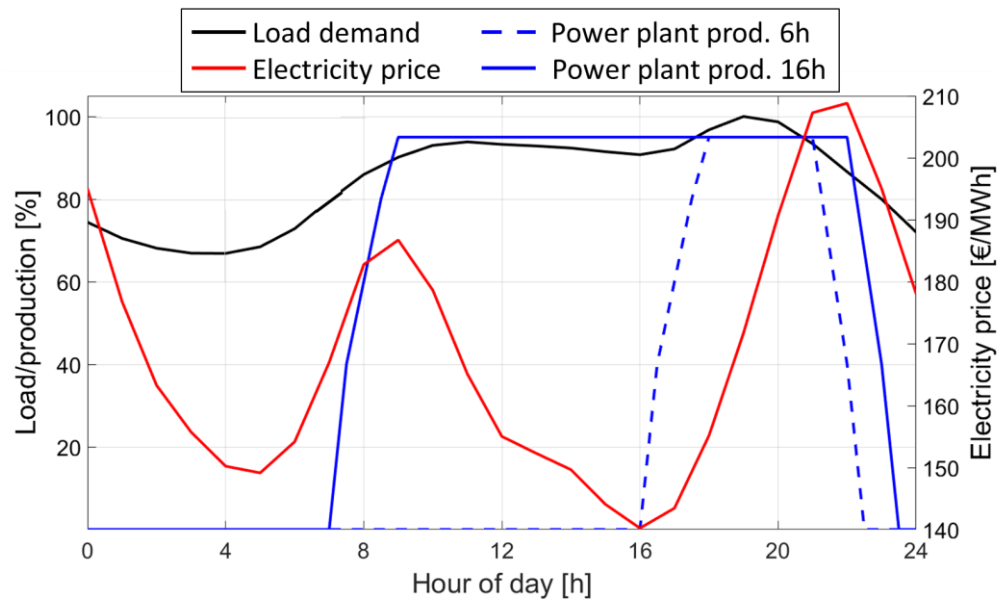
PEM at part loads



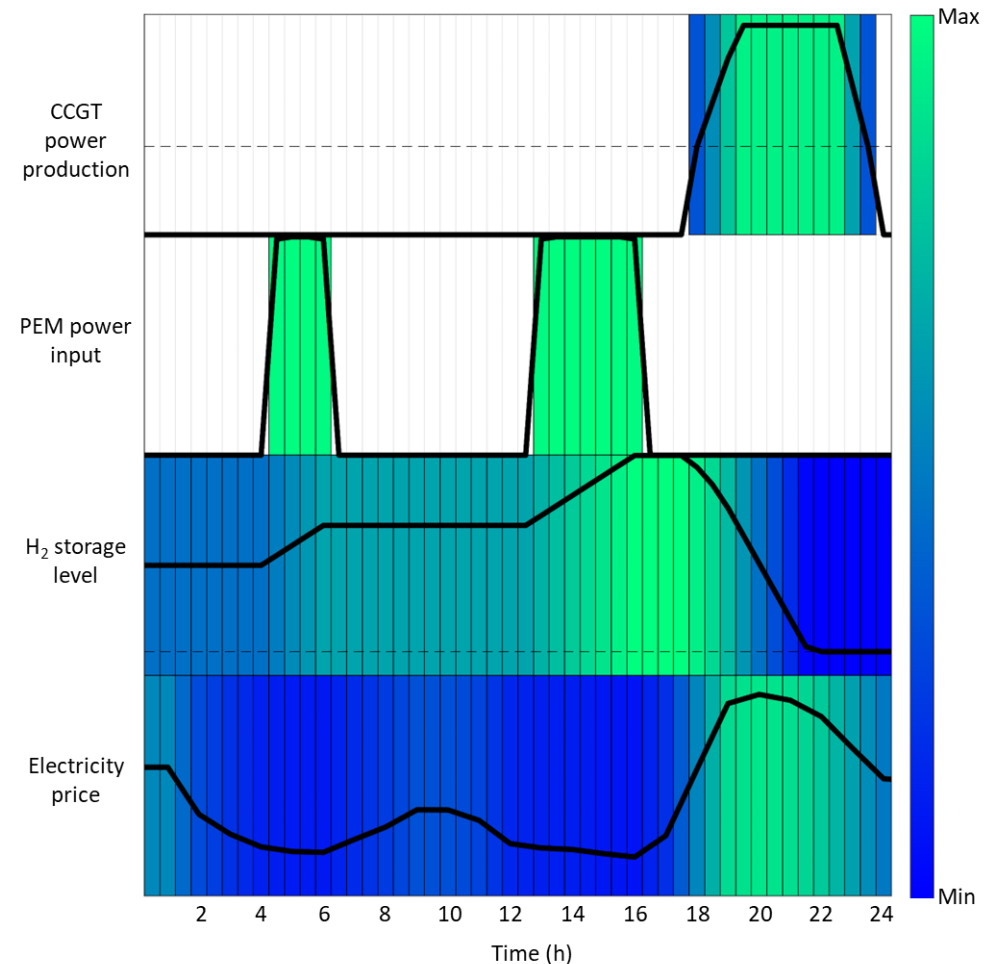


# The Model: Dispatch / control

## Electricity production Pre-defined profiles

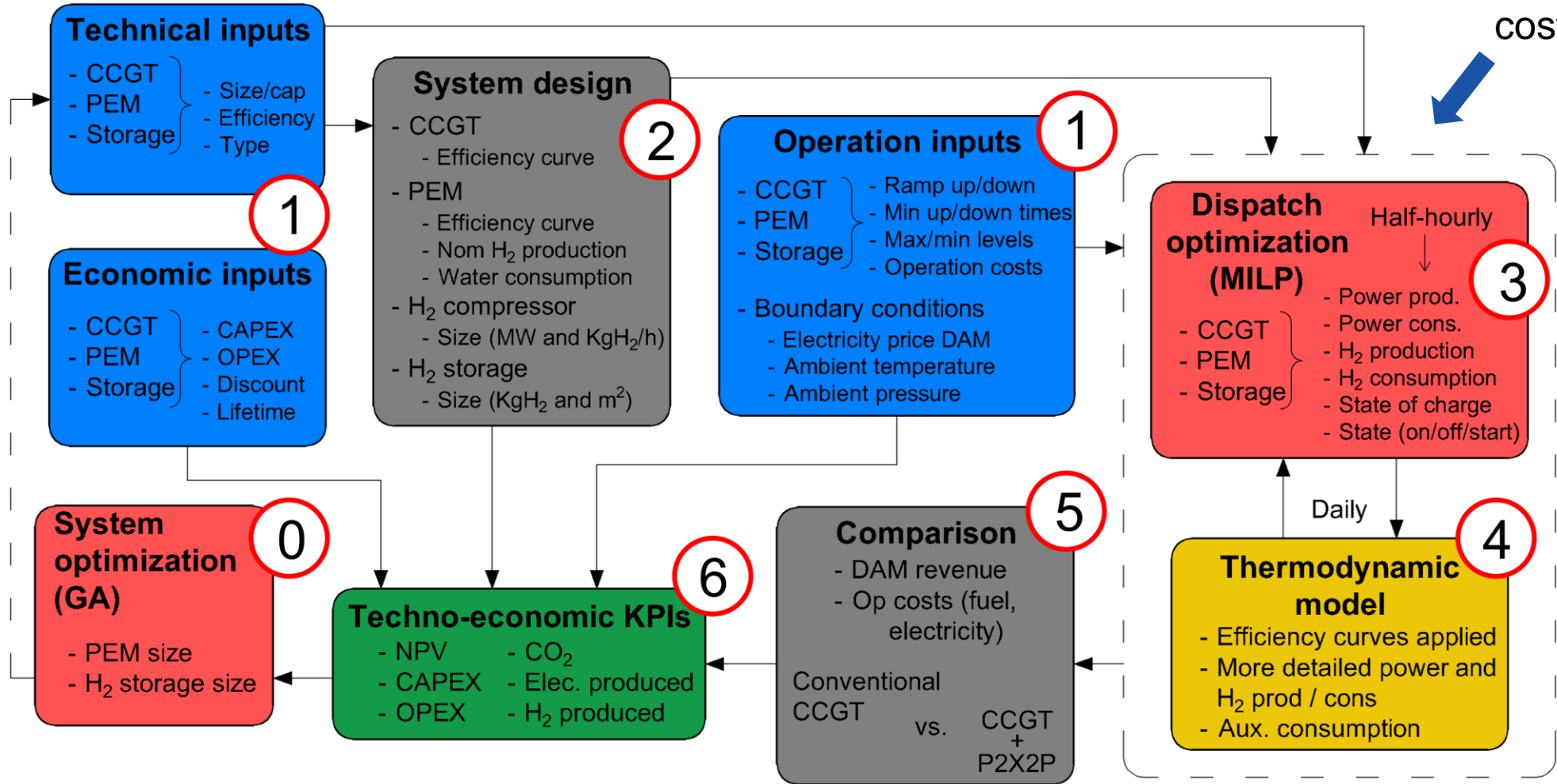


## Hydrogen production - MILP



# Simulation process

Minimize operational costs

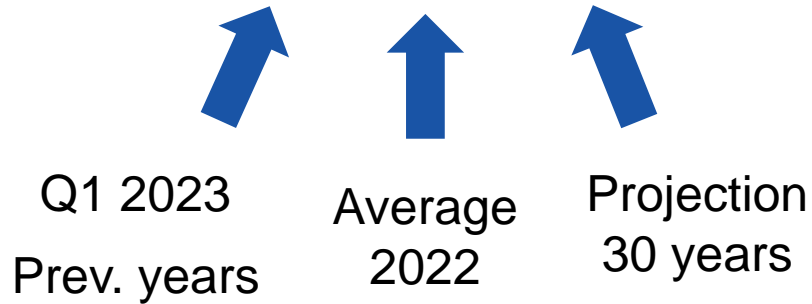


Objectives:  
 • Max NPV  
 • Min CO<sub>2</sub>

# Scenarios - results

## Fuel market scenarios

	Low	Medium	High
Natural gas [€/MWh]	50	130	210
CO <sub>2</sub> tax [€/ton]	40	80	120



## Results

- 12200 system configurations
  - Only 100 → H<sub>2</sub> production
  - Peaker plants perform better
  - Less than 150 hours per year
- 
- Added complexity / risk
    - Project execution
    - Control / operation
    - Combustion
    - Environment

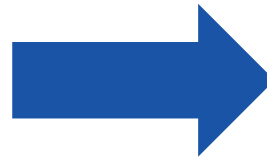


**Not  
feasible**

# Additional scenarios

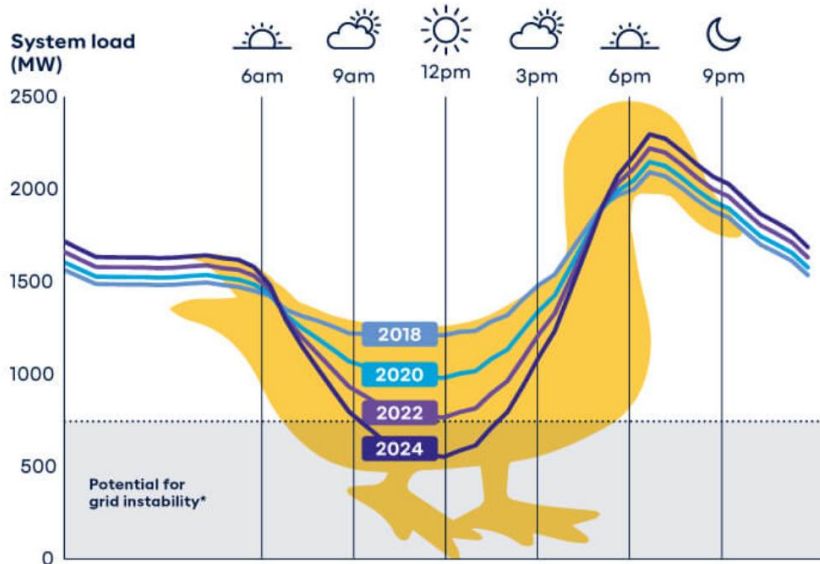
## Electricity demand

Duck curve

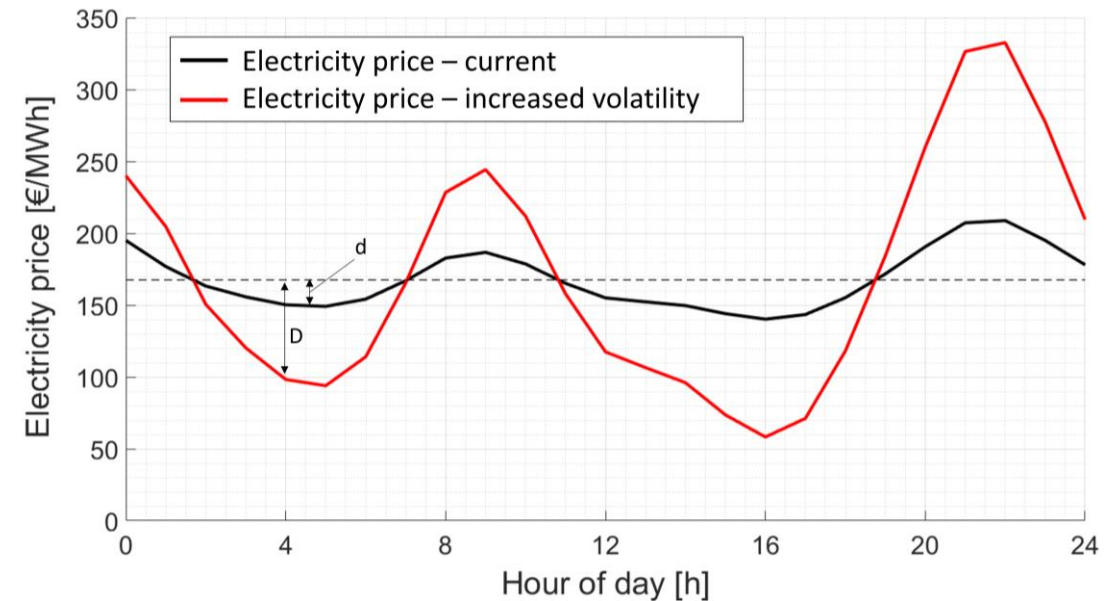


## Electricity Price

Increased price volatility



Source: www.synergy.net.au



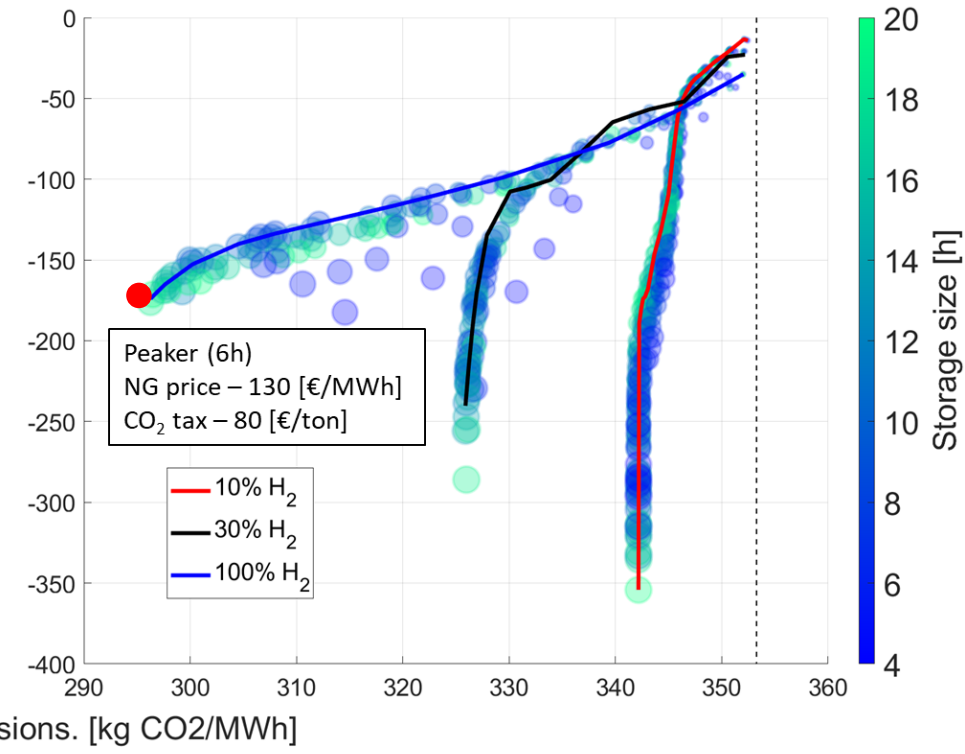
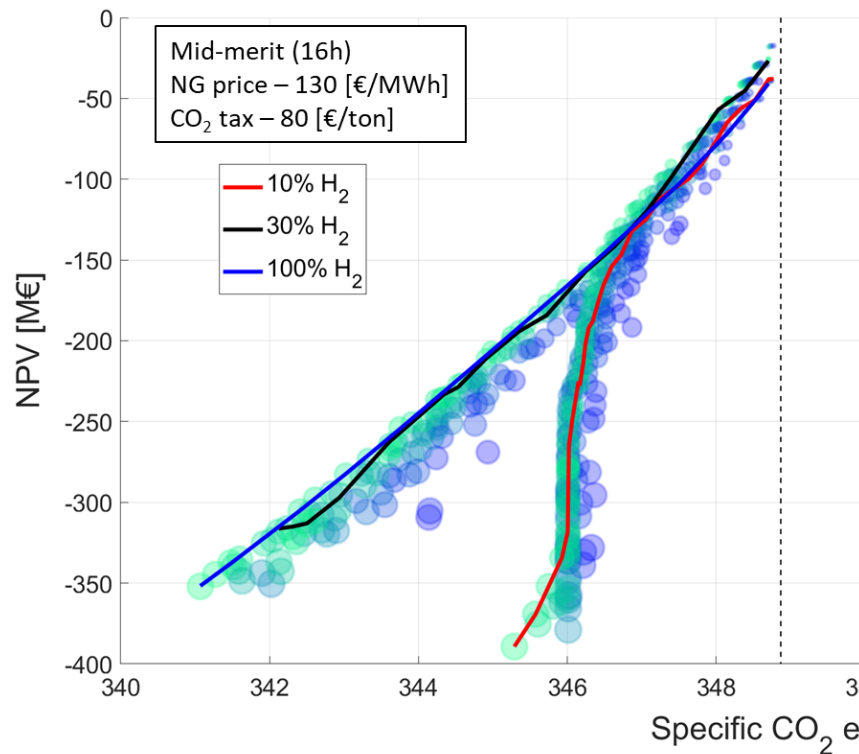
# Additional scenarios – medium fuel price

- Negative NPV
- Environmental impact
- Example configuration:
  - Peaker
  - PEM 390 MW<sub>e</sub>
  - Storage 19 h
  - 100% H<sub>2</sub>

Parameter	Units	Reference	Example config
NG cons.	[kton NG]	87.54	73.41
NG price	[€/MWh]	130	
Cost NG	[M€]	158.14	132.62
Elec prod.	[GWh]	681.42	
Elec purch.	[GWh]	0	267.70
Cost Elec	[M€]	0	1.24
PEM OH	[h]	0	696.00
H2 prod.	[kton H <sub>2</sub> ]	0	5.03
NPV	[M€]	0	-176.13
spf. CO <sub>2</sub>	[kg/MWh]	353.27	296.26

Specific CO <sub>2</sub> emissions [kgCO <sub>2</sub> /MWh]				
	BAU	10% H <sub>2</sub>	30% H <sub>2</sub>	100% H <sub>2</sub>
	348.9	345.3	342.1	341.1
		-1.0 %	-1.9 %	-2.2 %

Specific CO <sub>2</sub> emissions [kgCO <sub>2</sub> /MWh]				
	BAU	10% H <sub>2</sub>	30% H <sub>2</sub>	100% H <sub>2</sub>
	353.2	342.2	325.9	296.3
		-1.9 %	-6.6 %	-15.1 %



# Additional scenarios – high fuel price

- Example configuration:
  - Peaker
  - PEM 380 MW<sub>e</sub>
  - Storage 11 h
  - 100% H<sub>2</sub>

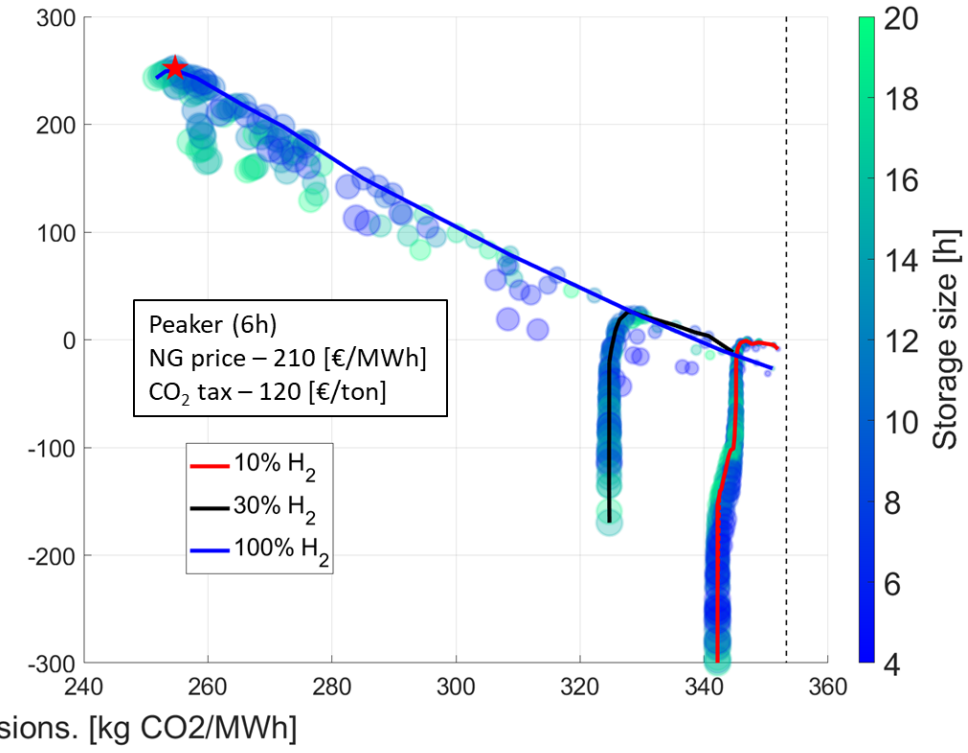
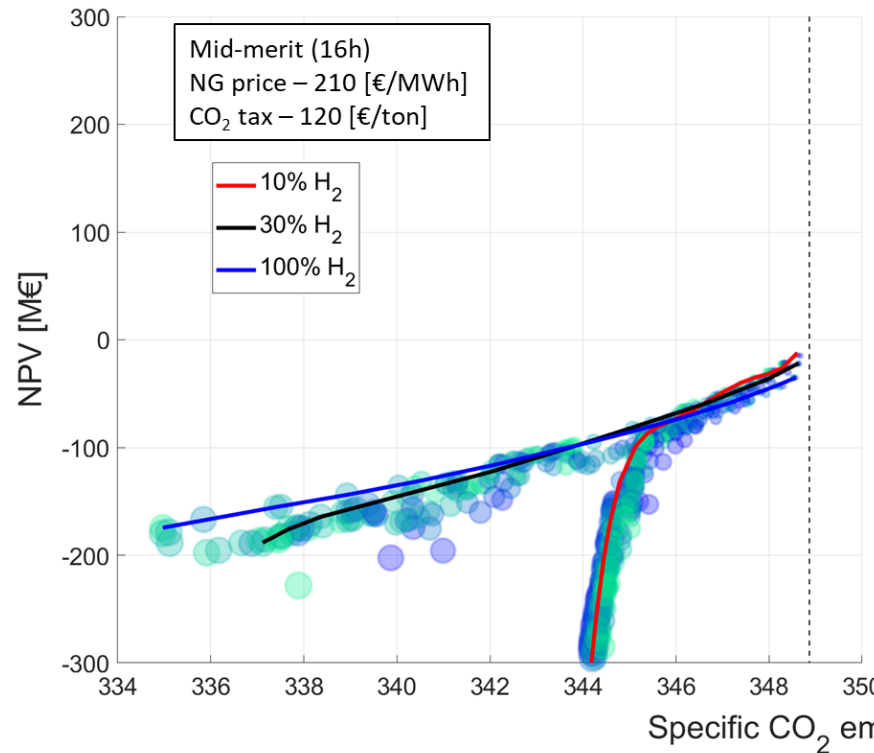
Parameter	Units	Reference	Example config
NG cons.	[kton NG]	87.5	63.1
NG price	[€/MWh]	210	
Cost NG	[M€]	255.5	184.2
Elec prod.	[GWh]	681.4	
Elec purch.	[GWh]	0	511.0
Cost Elec	[M€]	0	15.7
PEM OH	[h]	0	1338
H2 prod.	[kton H2]	0	9.6
NPV	[M€]	0	251.9
spf. CO <sub>2</sub>	[kg/MWh]	353.3	254.7
PEM area	[m <sup>2</sup> ]	0	5651
Storage area	[m <sup>2</sup> ]	0	3152.8
Storage cap.	[ton H2]	0	79.2
Water cons.	[m <sup>3</sup> ]	0	143986

PEM OH: 500 h

CO<sub>2</sub>: 349 → 335 [Kg/MWh] -4%

PEM OH: 1340 h

CO<sub>2</sub>: 353 → 255 [Kg/MWh] -30%



# Conclusions

Layout proposed: CCGT + electrolyser with storage – P2X2P

Not feasible under current fuel and electricity markets

## Challenges

- Technology readiness
- Large investment
- Footprint
- Water consumption

Potential in a scenario with  
greater electricity price volatility

